

Optimization of the NO_x reduction condition in the combustion furnace for the combustion of "heavy-oil - NH₃ system" using CFD

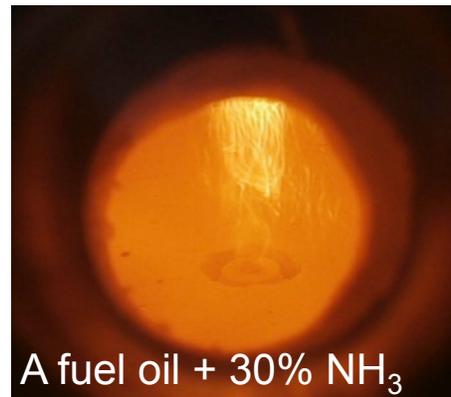
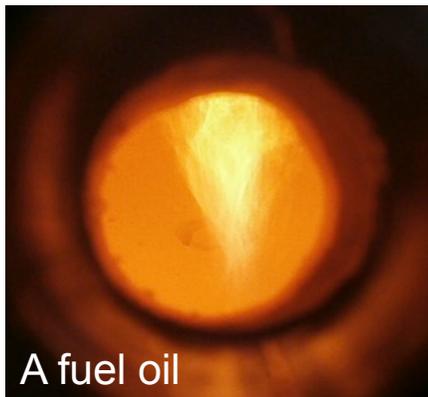
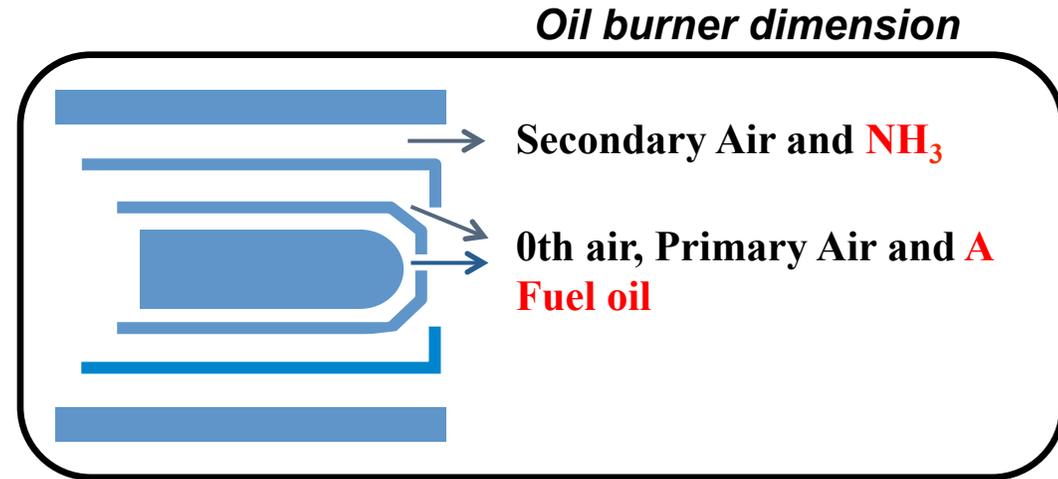
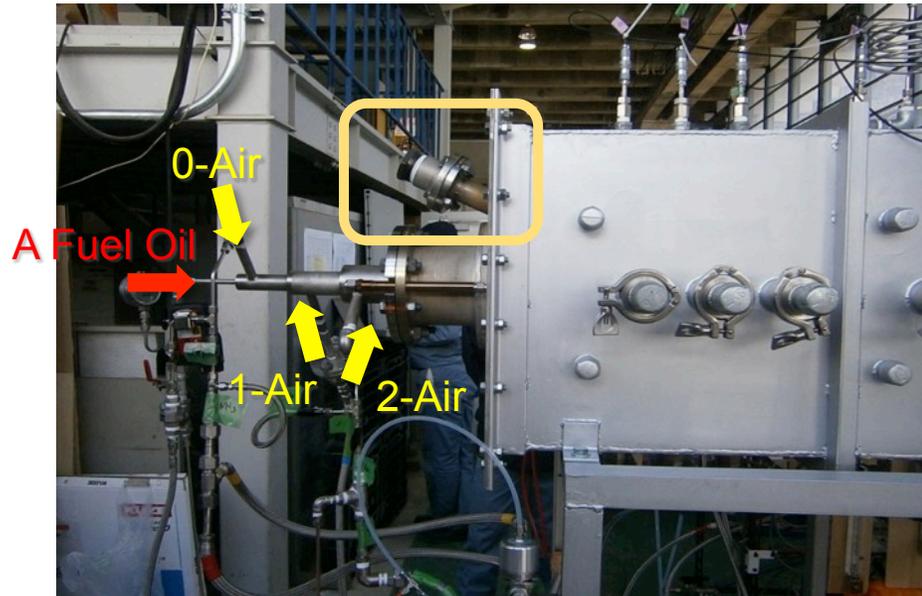
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A Fuel Oil-NH₃ co-combustion experiments

10kW Furnace (Inner : L.1200 mm×H.300mm×W.300mm)



$$\lambda(\text{total air/theoretical air for Fuel})=1.05-1.3$$

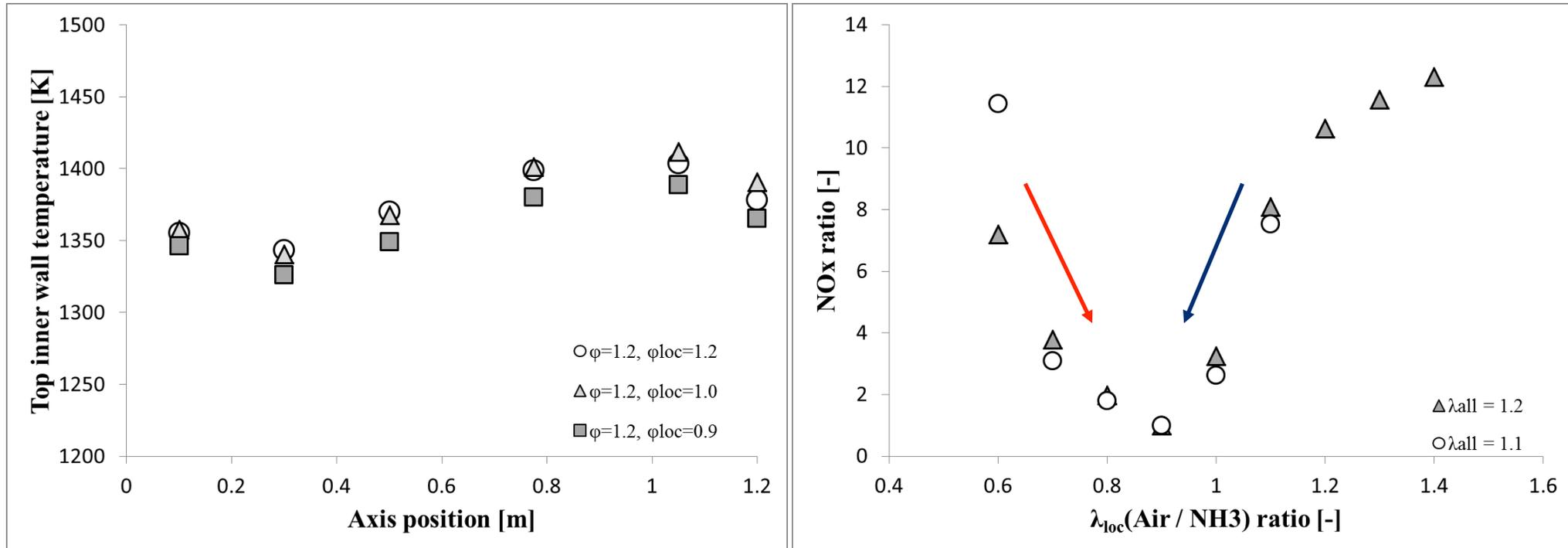
$$\lambda_{\text{loc}}(\text{secondary air/theoretical air for NH}_3)=0.6-1.4$$

λ_{loc} is most important parameter for NO_x reduction.

Experimental results

When NH_3 mixing rates increased in this study, the temperature distribution in the furnace decreased. N_2 increase in exhaust gas composition and a decrease in CO_2 influence it.

In addition, we discovered that there was a NO_x reduction effect when we regulated transportation atmosphere for an NH_3 supply line to show it in the right figure.



Inner wall temperature distribution [K]

NO_x ratio for λ_{loc} [-]

Turbulence Combustion Model (EDC)

Species transport equations

$$\frac{\partial}{\partial t} (\rho Y_{li}) + \nabla \cdot (\rho \mathbf{v} Y_{li}) = -\nabla \cdot \mathbf{J}_{li} + R_{li} \quad Y_{li} \downarrow \uparrow^* = Y_{li} + \int_0^{\tau^*} \sum_{r=1}^N \frac{R_{li,r}}{\rho} dt$$

Chemical reaction equations

Volume fraction constant:

$$\sum_{i=1}^N \nu_{li,r} M_{li} \Leftrightarrow k_{f,r} / k_{b,r} + \sum_{i=1}^N \nu_{li,r}' M_{li} \quad \xi^* = C_{\xi} \left(\nu \varepsilon / \kappa^2 \right)^{1/4}, \quad C_{\xi} = 2.1377$$

Time scale constant:

$$\tau^* = C_{\tau} (\nu / \varepsilon)^{1/2}, \quad C_{\tau} = 0.4082$$

Net reaction rates [1]

$$R_{li} = \rho (\xi^*)^2 / \tau^* [1 - (\xi^*)^3] (Y_{li} \downarrow \uparrow^* - Y_{li}) \quad \text{kinematic viscosity: } \nu = \mu / \rho \text{ [m}^2 \text{/s]}$$

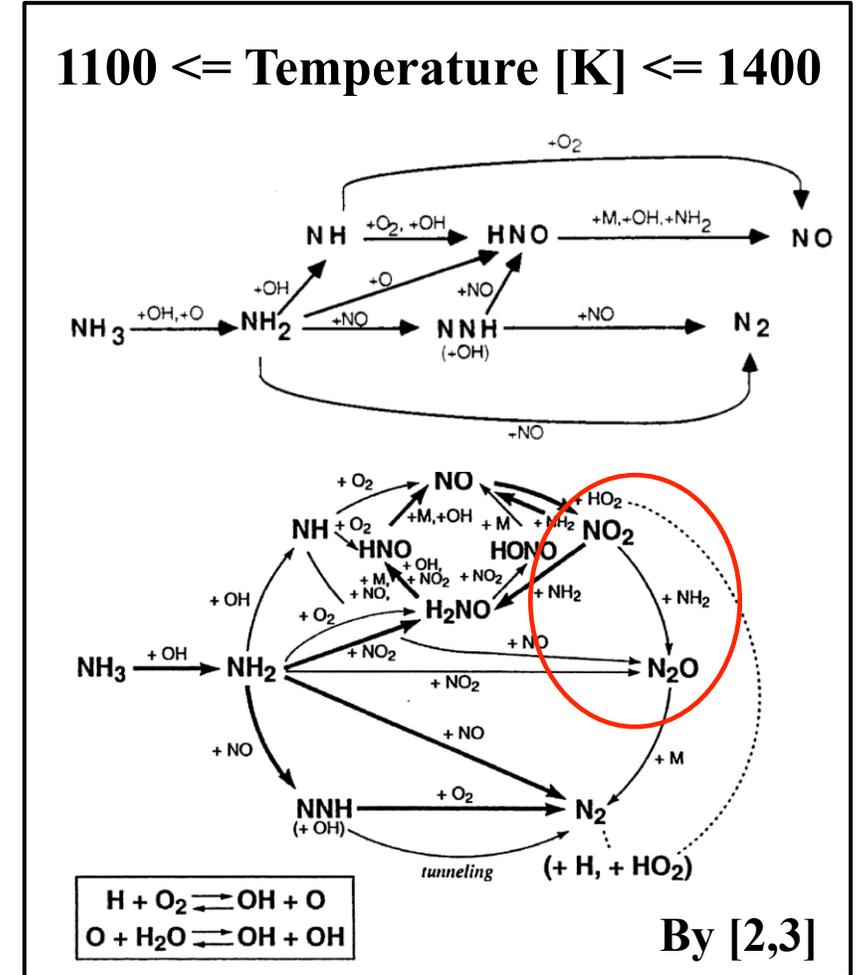
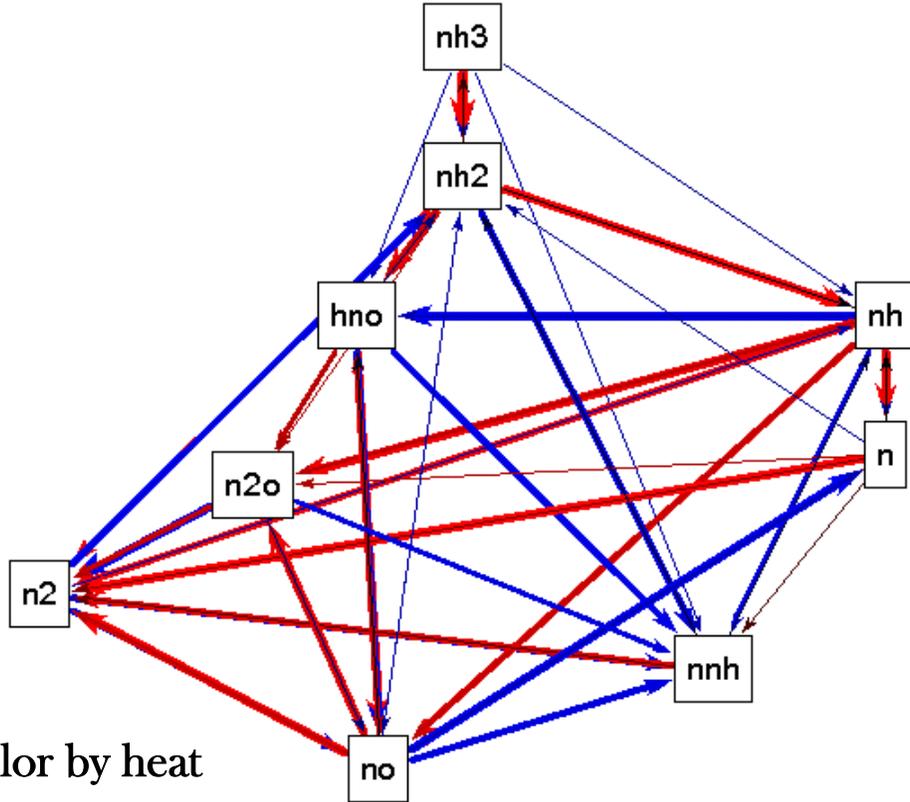
Because some slow reactions exist, it is difficult to solve the reaction term.

By the direct integration for fine scales, it is considered chemical reaction and turbulence mixing at the same time.

[1] Magnussen : On the structure of Turbulence and a generalized Eddy Dissipation Concept for chemical reaction in turbulent flow (1981)

NH₃ Combustion & Fuel NO_x (Simplified Miller's Mechanism)

Reaction path for the oxidation of ammonia in flames.

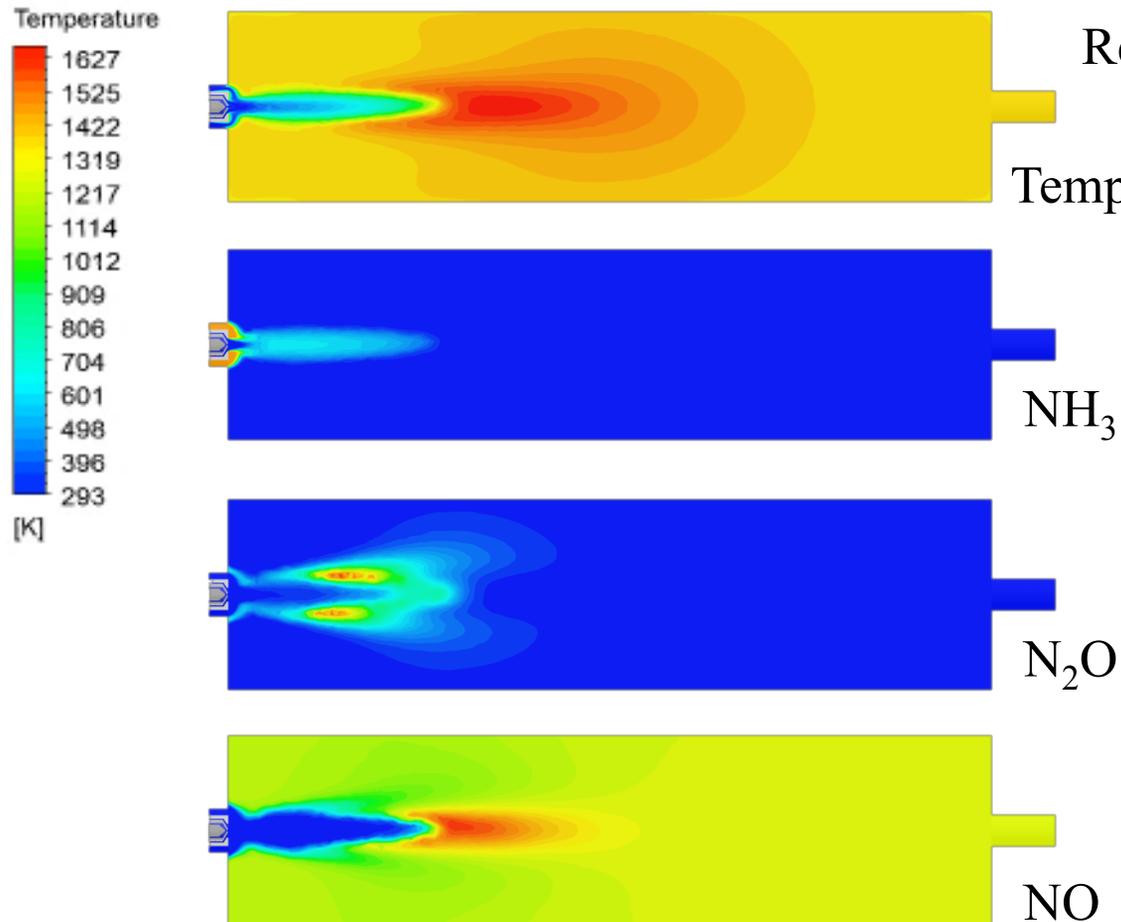


[2] James A. Miller : Mechanism and Modeling of Nitrogen Chemistry in Combustion(1989)

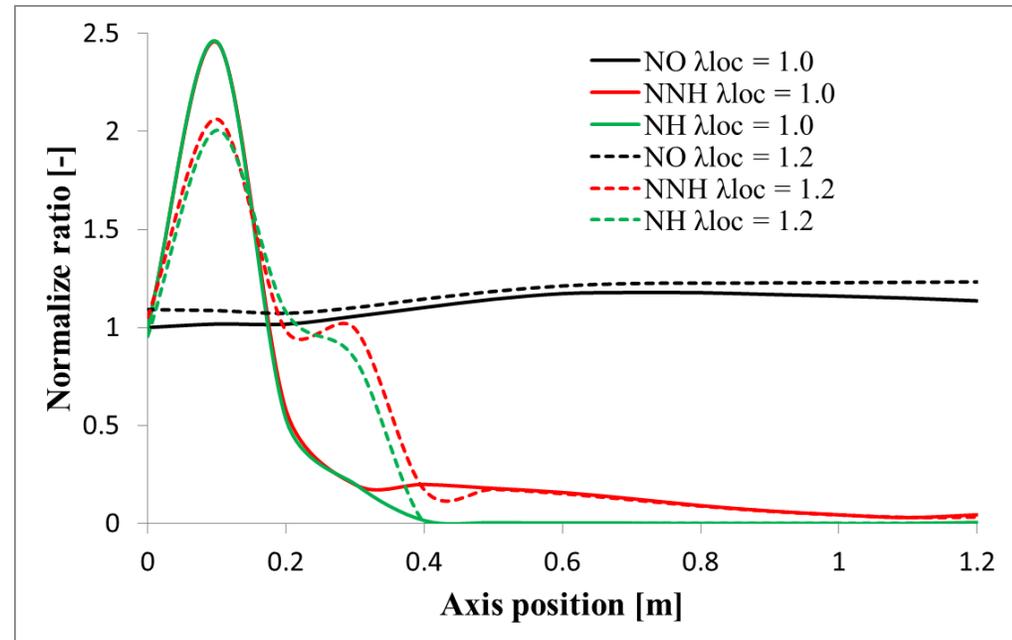
[3] James A. Miller : Modelling the Formation of N₂O and NO₂ in the Thermal De-NO_x Process (1996)

CFD results

A difference became less than the experimental results in the NH_3 reaction mechanism which I used in this study. I am inspecting how there is influence of the reaction mechanism that I simplified.

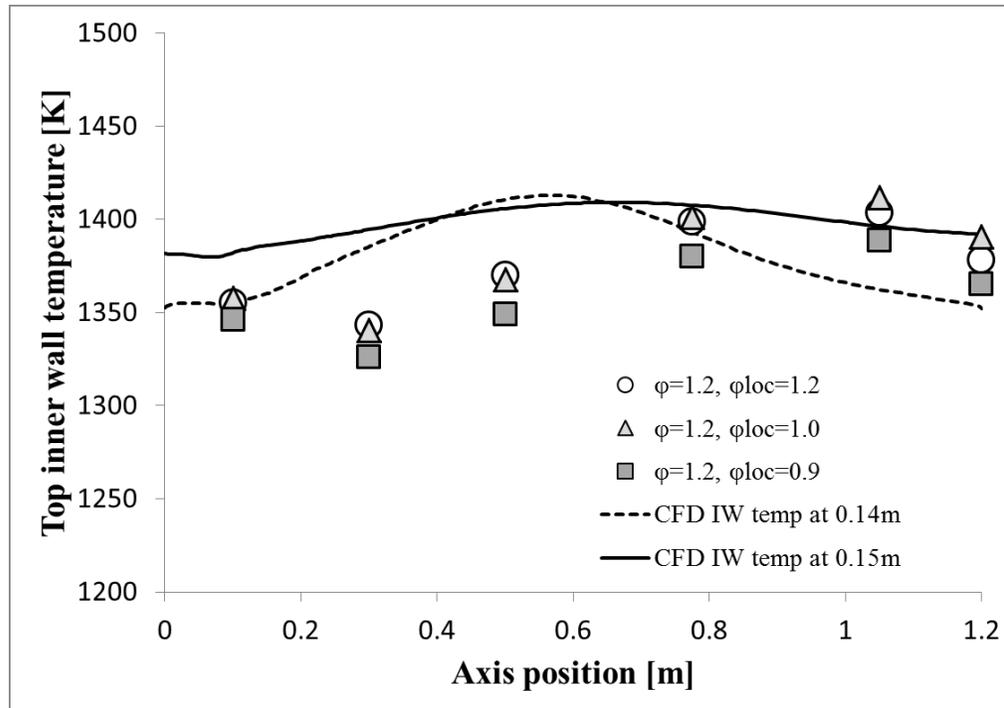


Results of contour for $\lambda=1.2$, $\lambda_{\text{loc}}=1.2$

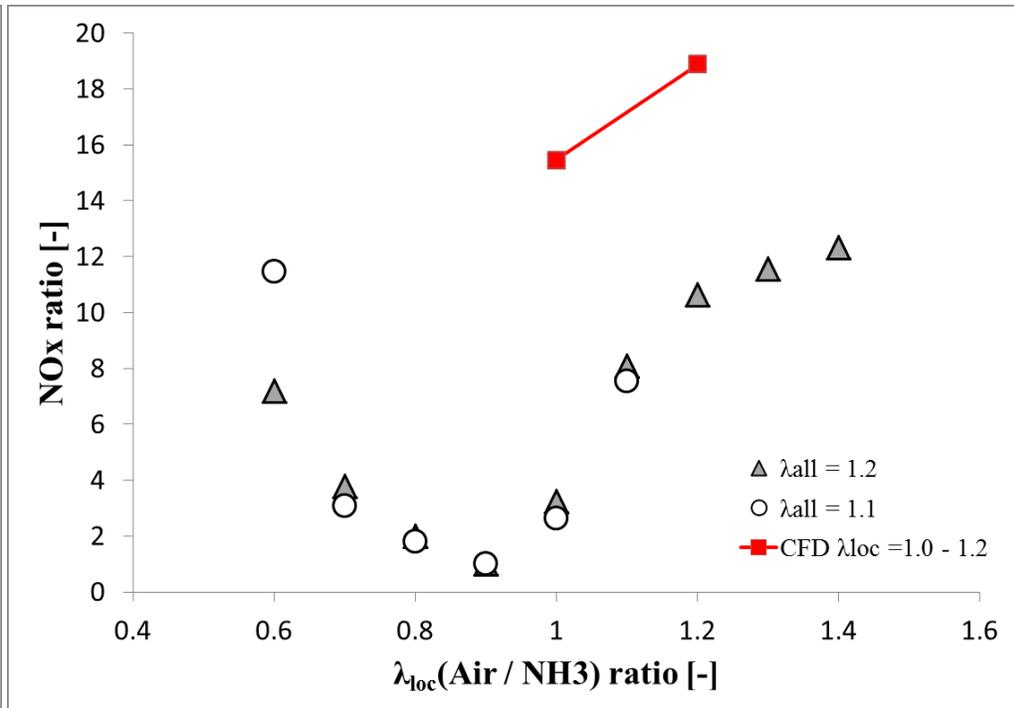


Conclusion

We inspected it about NO_x behavior of A Fuel oil–NH₃ co-combustion by experiment and CFD. We understood that there was a local minimum of the NO_x by the experiment. On the other hand, the analysis result by CFD became higher in NO_x concentration than some experiments. According to the precision of simplification of the reaction mechanism and the analysis model, this is thought about. We will do the study continuously in the future to raise precision more.



Inner wall temperature distribution [K]



NO_x ratio for λ_{loc} [-]

Thank you for your attention.

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