

# Optimization of the NO<sub>x</sub> reduction condition in the combustion furnace for the combustion of "heavy-oil - NH<sub>3</sub> system" using CFD

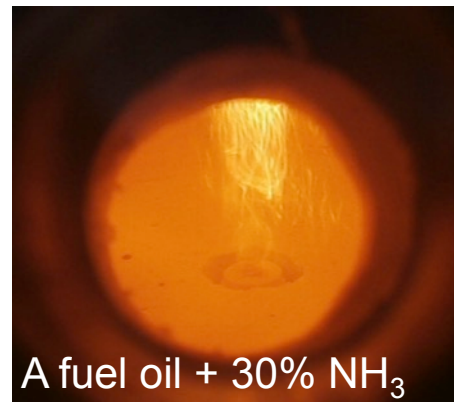
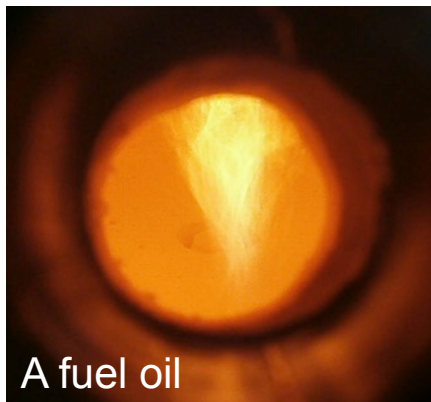
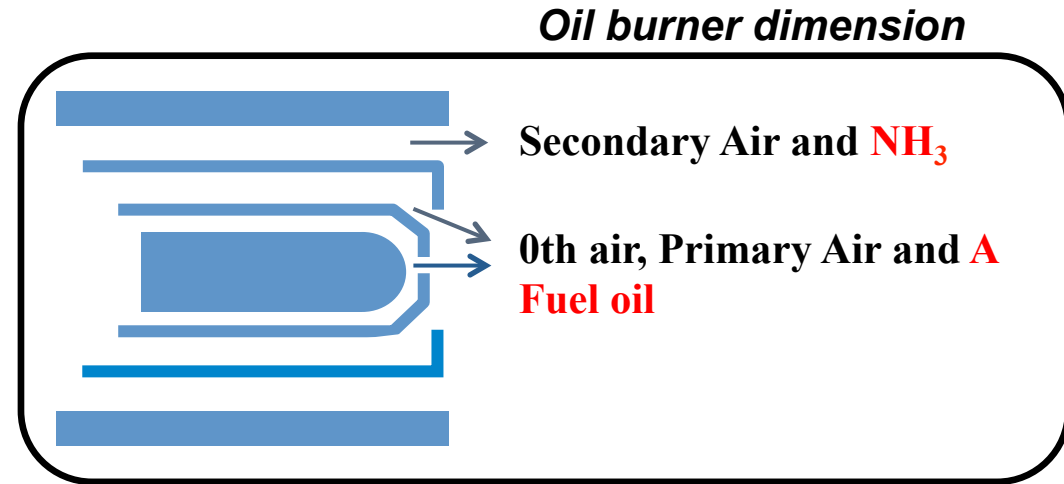
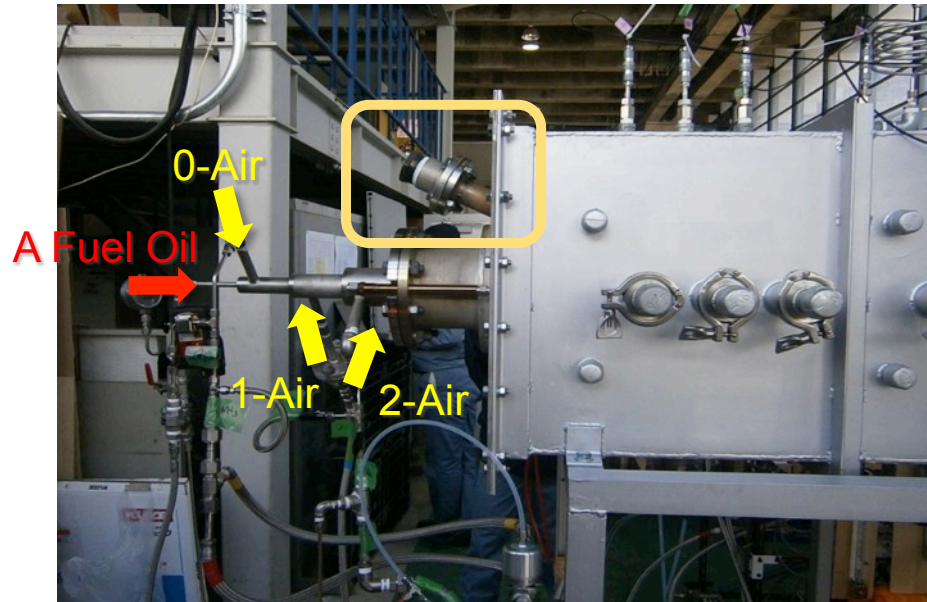
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# A Fuel Oil-NH<sub>3</sub> co-combustion experiments

10kW Furnace (Inner : L.1200 mm×H.300mm×W.300mm)



$$\lambda(\text{total air/theoretical air for Fuel})=1.05-1.3$$

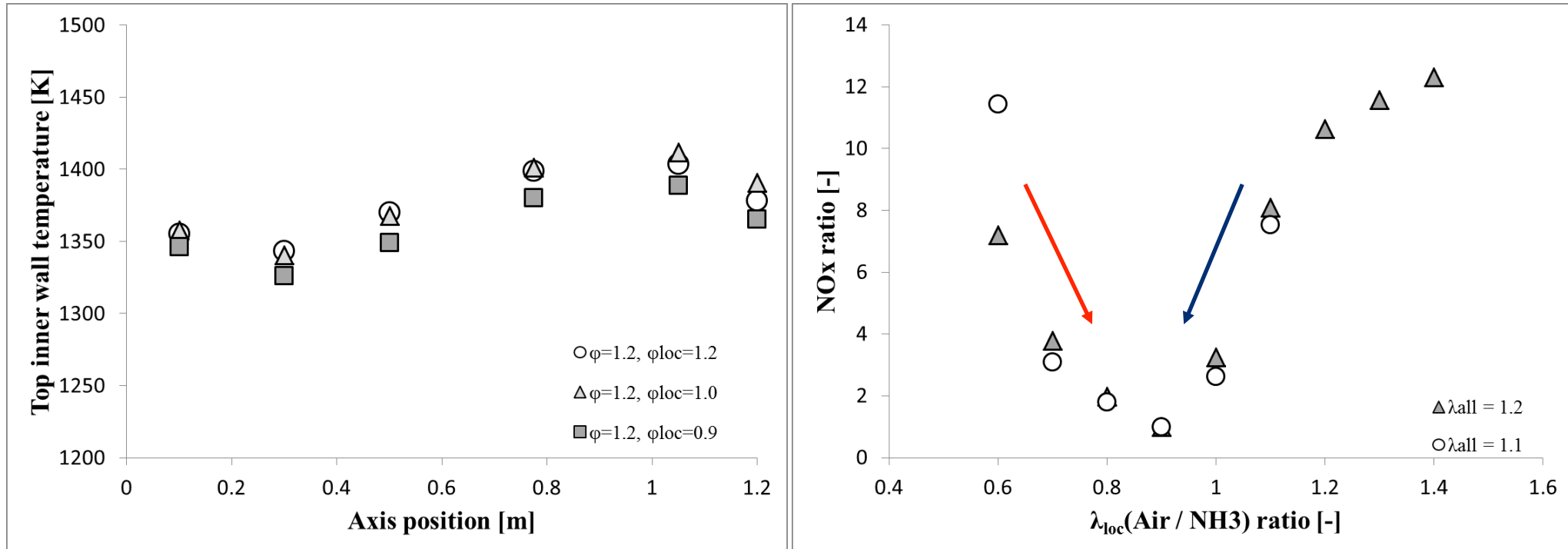
$$\lambda_{\text{loc}}(\text{secondary air/theoretical air for NH}_3)=0.6-1.4$$

$\lambda_{\text{loc}}$  is most important parameter for NO<sub>x</sub> reduction.

# Experimental results

When  $\text{NH}_3$  mixing rates increased in this study, the temperature distribution in the furnace decreased.  $\text{N}_2$  increase in exhaust gas composition and a decrease in  $\text{CO}_2$  influence it.

In addition, we discovered that there was a  $\text{NO}_x$  reduction effect when we regulated transportation atmosphere for an  $\text{NH}_3$  supply line to show it in the right figure.



Inner wall temperature distribution [K]

$\text{NO}_x$  ratio for  $\lambda_{loc}$  [-]

# Turbulence Combustion Model (EDC)

Species transport equations

$$\frac{\partial}{\partial t} (\rho Y_i) + \nabla \cdot (\rho \mathbf{v} Y_i) = -\nabla \cdot \mathbf{J}_i + R_i \quad Y_i \downarrow \uparrow^* = Y_i + \int_0^{\tau^*} \sum_{r=1}^N \frac{R_{i,r}}{\rho} dt$$

Chemical reaction equations

Volume fraction constant:

$$\sum_{i=1}^N \nu_{i,r} M_i \Leftrightarrow k_{f,r} / k_{b,r} + \sum_{i=1}^N \nu_{i,r} \frac{\rho_i}{\rho} \frac{M_i}{\xi} \left( \nu \varepsilon / \kappa^2 \right)^{1/4}, C_\xi = 2.1377$$

Time scale constant:

$$\tau^* = C_\tau (\nu / \varepsilon)^{1/2}, C_\tau = 0.4082$$

Net reaction rates [1]

$$R_i = \rho (\xi^*)^2 / \tau^* [1 - (\xi^*)^3] (Y_i \downarrow \uparrow^* - Y_i)$$

kinematic viscosity:  $\nu = \mu / \rho$  [m<sup>2</sup>/s]

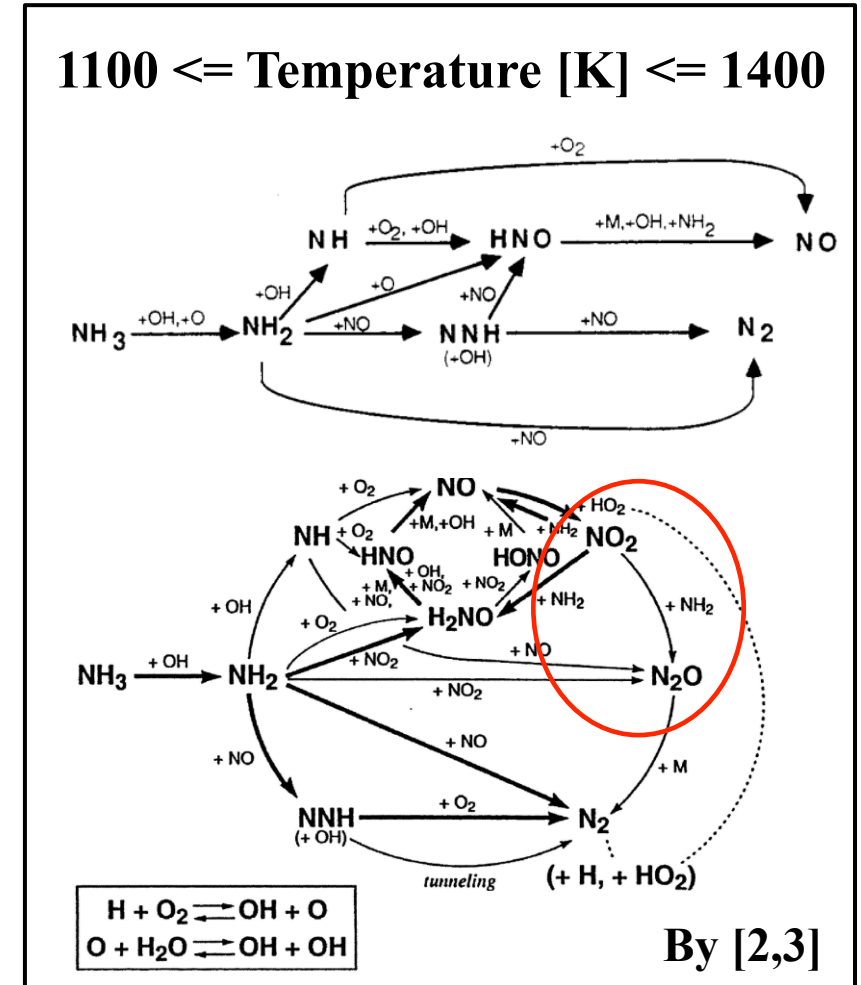
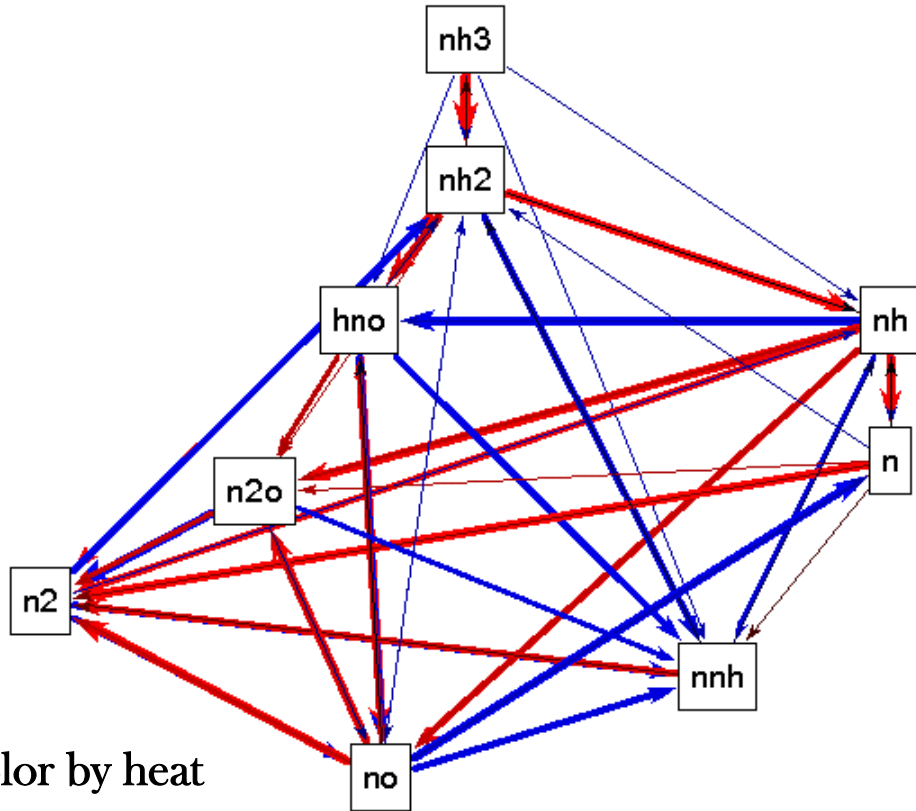
Because some slow reactions exist, it is difficult to solve the reaction term.

By the direct integration for fine scales, it is considered chemical reaction and turbulence mixing at the same time.

[1] Magnussen : On the structure of Turbulence and a generalized Eddy Dissipation Concept for chemical reaction in turbulent flow (1981)

# NH<sub>3</sub> Combustion & Fuel NO<sub>x</sub> (Simplified Miller's Mechanism)

Reaction path for the oxidation of ammonia in flames.

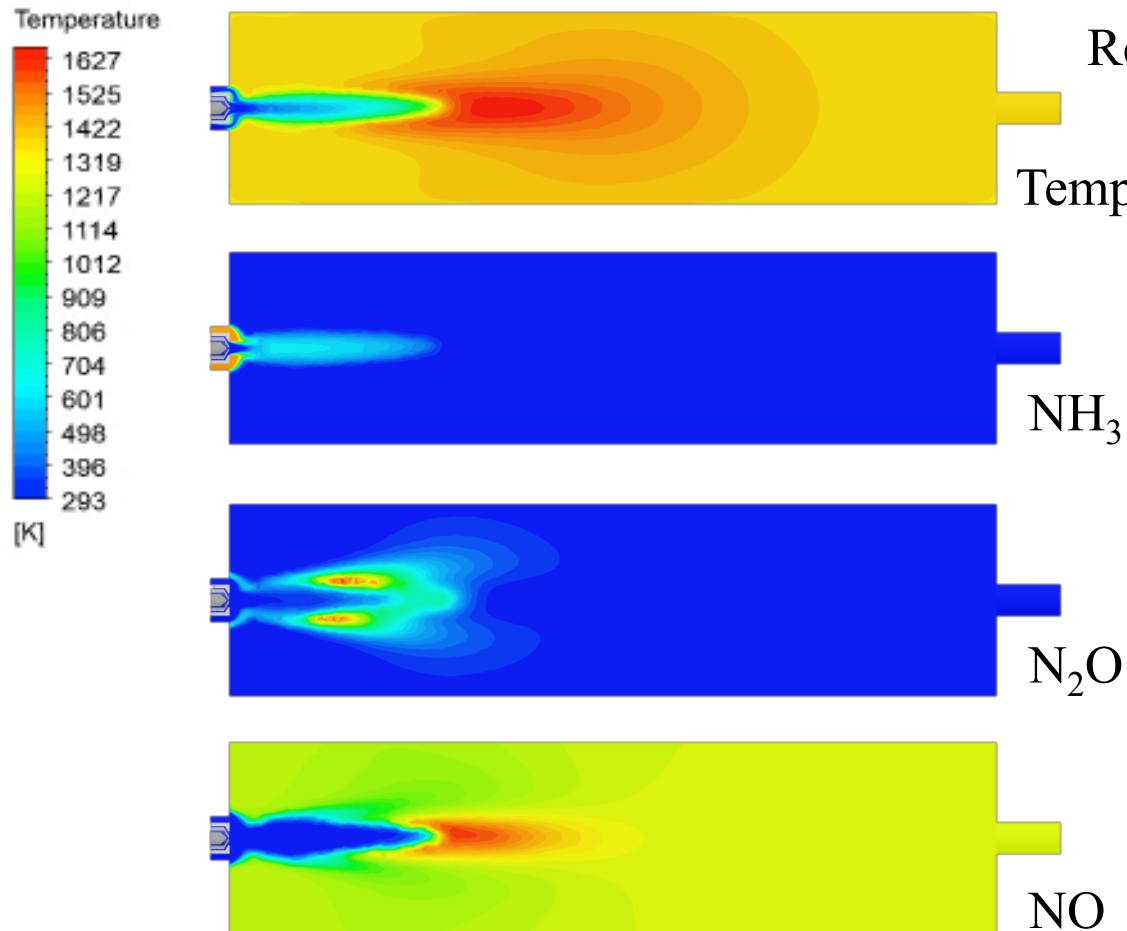


[2] James A. Miller : Mechanism and Modeling of Nitrogen Chemistry in Combustion(1989)

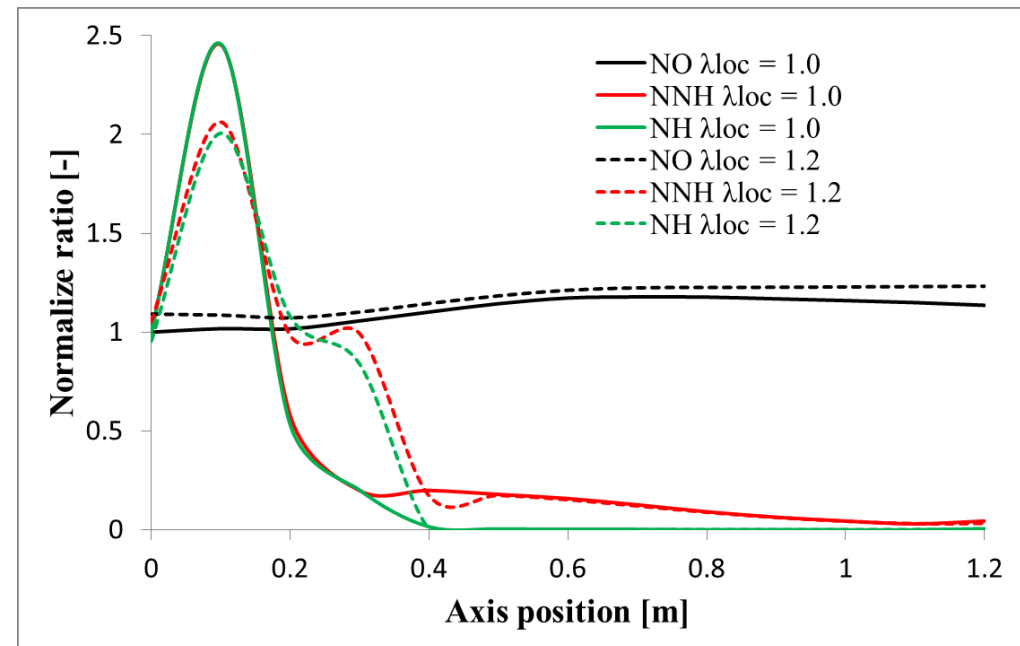
[3] James A. Miller : Modelling the Formation of N<sub>2</sub>O and NO<sub>2</sub> in the Thermal De-NO<sub>x</sub> Process (1996)

# CFD results

A difference became less than the experimental results in the  $\text{NH}_3$  reaction mechanism which I used in this study. I am inspecting how there is influence of the reaction mechanism that I simplified.

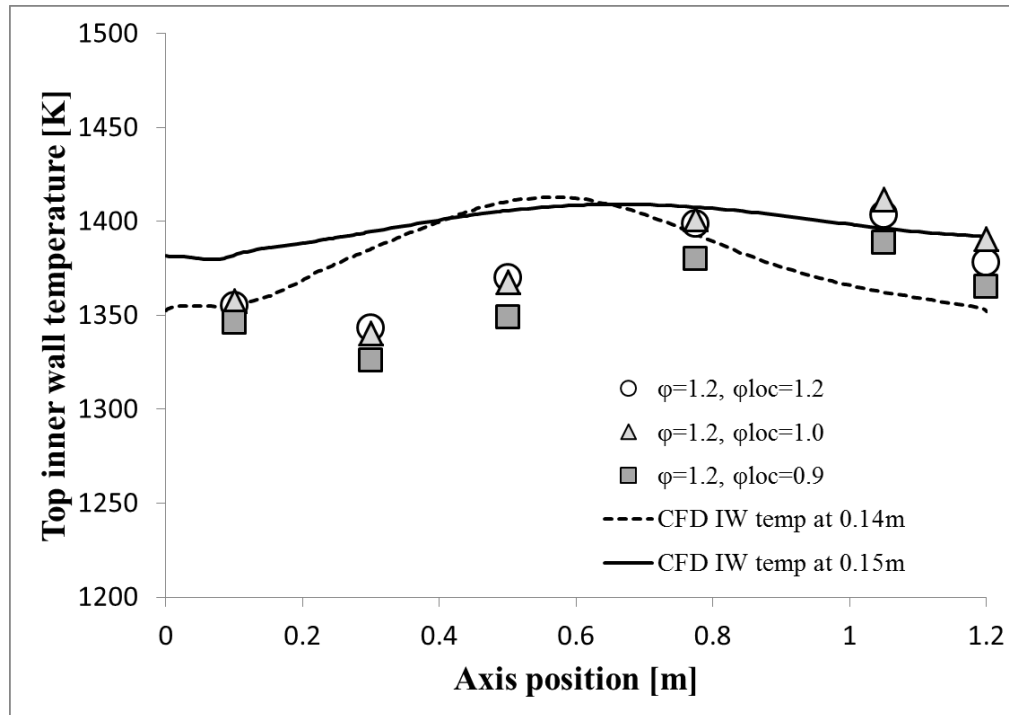


Results of contour for  $\lambda=1.2$ ,  $\lambda_{\text{loc}}=1.2$

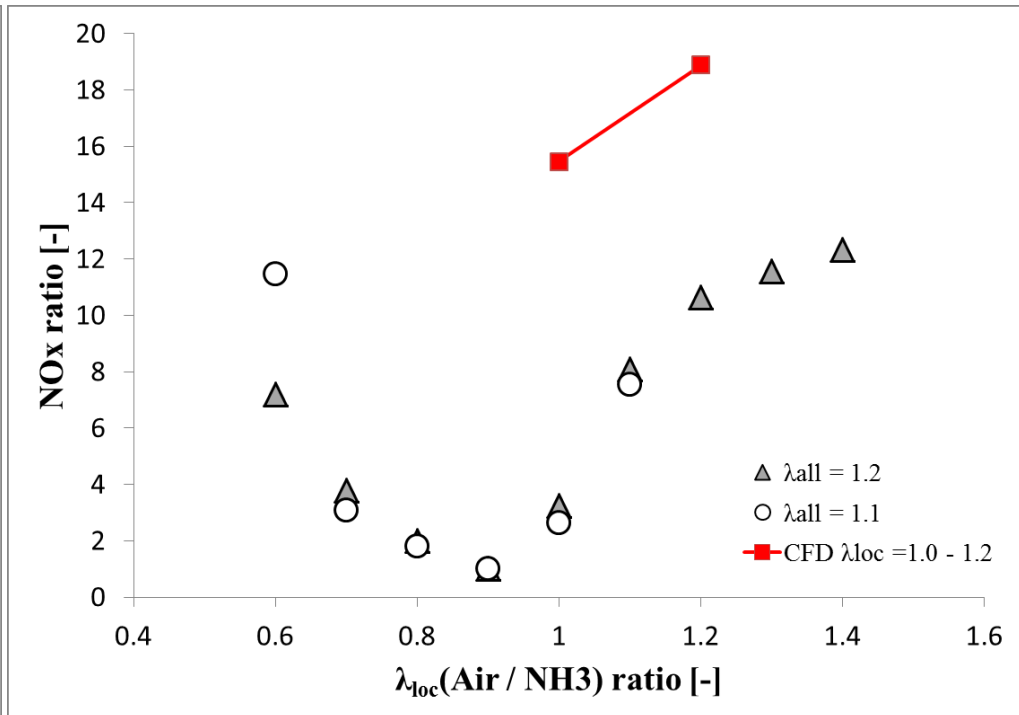


# Conclusion

We inspected it about NO<sub>x</sub> behavior of A Fuel oil–NH<sub>3</sub> co-combustion by experiment and CFD. We understood that there was a local minimum of the NO<sub>x</sub> by the experiment. On the other hand, the analysis result by CFD became higher in NO<sub>x</sub> concentration than some experiments. According to the precision of simplification of the reaction mechanism and the analysis model, this is thought about. We will do the study continuously in the future to raise precision more.



Inner wall temperature distribution [K]



NO<sub>x</sub> ratio for  $\lambda_{loc}$  [-]

*Thank you for your attention.*

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