

The Ammonia Economy Global Potential and Possible Pathways

NH3FUEL CONFERENCE DES MOINES, IA SEPTEMBER, 2014

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The Prize – 21st Century

(With Apologies to Daniel Yergin)

A zero carbon fuel

That can be used for transportation and power generation

That is scalable from global chemical to global energy proportions

That is an inherently clean fuel with regard to traditional pollutants and CO₂

That has a century long history of large scale handling and use

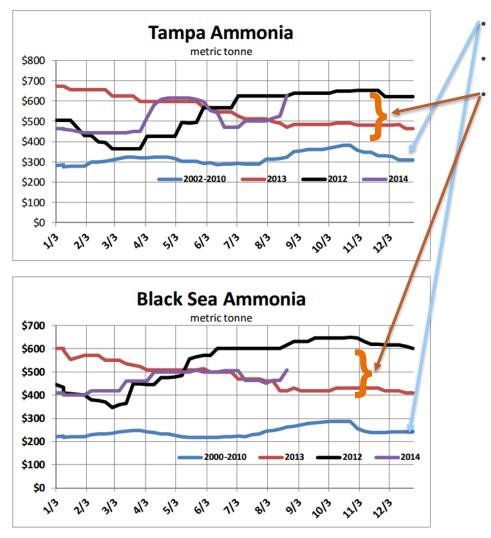
That is competitive in energy pricing to current fuels

That holds promise for low or no carbon production (through CCS on standard technology or advanced technology for renewables or nuclear)

That *appears to be* within easy reach through optimization of production, use and safety regulations



Price History - Ammonia Industry

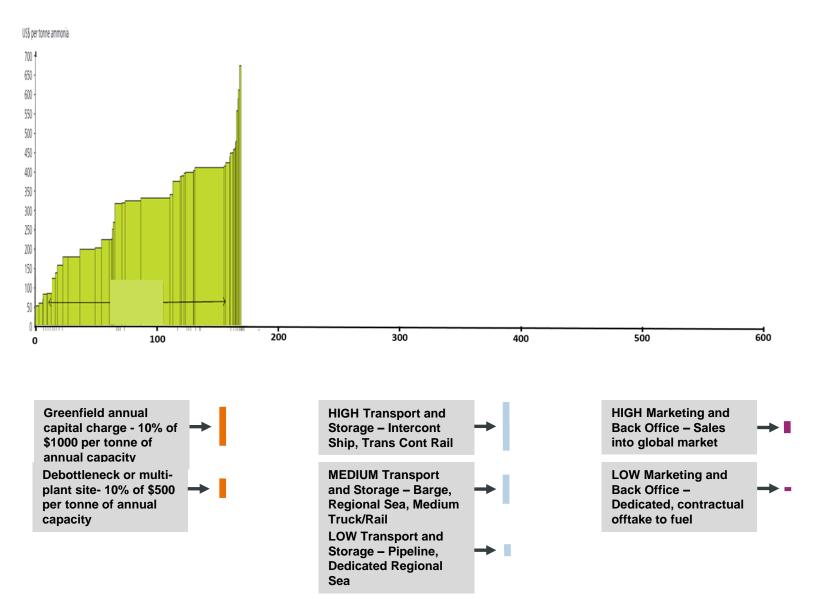


- 2002 2010 \$200 \$350
- US Mainland about \$100 higher
 - 2012 2014 \$350 \$650

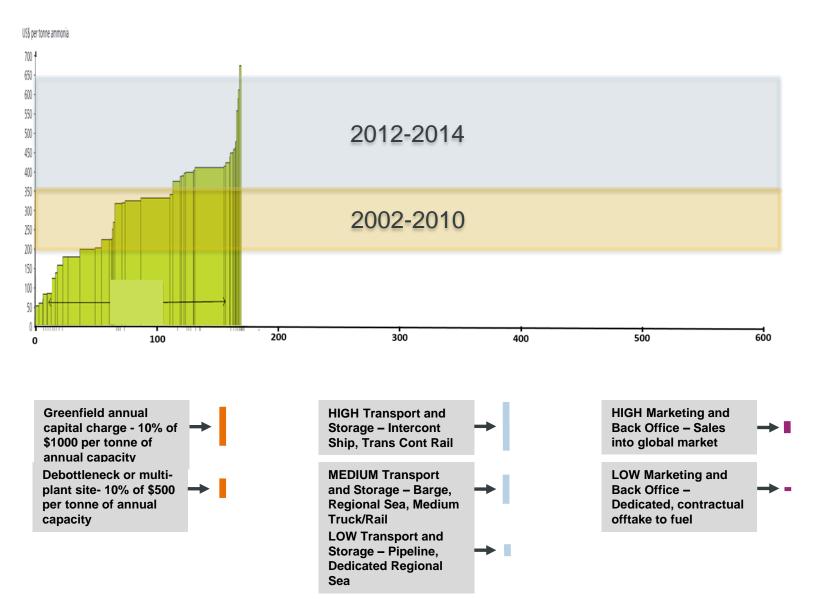


http://farmfutures.com/mdfm/Faress1/author/252/2014/8/WFertR081914.pdf

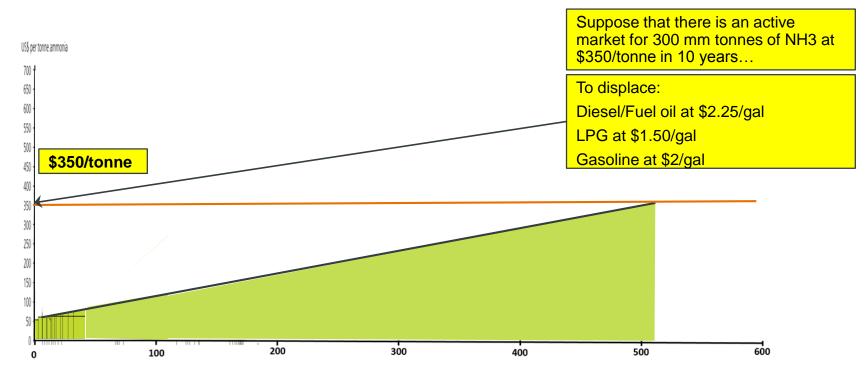
General Cost Structure of Ammonia Industry



Historical Price Ranges



What Happens with a Growing Fuels Market?



• Will there be ammonia to supply such a market?

| MODEL RESULTS | | | | | | | | | | | |
|---|------------------------------------|---|---|-----------------|--|--|--|--|--|--|--|
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | c | ALL VALUES ORRESPOND TO CASE PARAMETERS | | | | | | | | |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | | 5.86E+06 | | | | | | | | |
| OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NH3 BASIS) IN CS. ITERATE DA TO ACHIEVE DESIRED QUANTITY IN DS | | | 0.00 | | | | | | | | |
| MMBTU (or 1000 CF gas equiv) contained in NH3 | 21.32 | | 124,987,434 | | | | | | | | |
| MMBTU gas required for NH3 | 32.0 | | 187,616,000 | | | | | | | | |
| TCF natural gas required for NH3 | 2.94E-08 | | 0.172 | | | | | | | | |
| Tonnes water produced from NH3 | 1.58E+00 | | 9,263,540 | | | | | | | | |
| # Global ammonia industry | 6.67E-09 | | 0.039 | | | | | | | | |
| # of World Scale NH3 Plants | 1.255-06 | | 7.33 | | | | | | | | |
| Number of 60,000 cbm vessels | 2.445-05 | | 143 | | | | | | | | |
| Number of 80 tonne railcar deliveries | 0.0125 | | 73,288 | | | | | | | | |
| # of 1 MM TPA NH3 pipeline | 1.005-06 | | 5.9 | 1 | | | | | | | |
| MWh from 45% efficient power plants | 2.81E+00 | | 16,475,030 | T C mi pr | | | | | | | |
| # of 10 MW plants that can be run for 1 year, 45% | 3.215-05 | | 188.0 | | | | | | | | |
| Equivalent # of 6 mtpa LNG train (BTU basis) | 6.87E-08 | | 0.40 | | | | | | | | |
| Tonnes LNG equivalent | 0.41 | | 2,403,830 | ŀ | | | | | | | |
| Metric Tonnes coal equiv | 1.04 | | 6,097,520 | | | | | | | | |
| Tonnes oil equivalent (TOE) | 0.500 | | 2,931,500 | 6 | | | | | | | |
| Tonnes resid equiv | 0.530 | | 3,107,390 | P | | | | | | | |
| Gal LPG equiv | 234 | | 1,371,942,000 | A | | | | | | | |
| Gal Gasoline equiv | 172 | | 1,008,436,000 | F | | | | | | | |
| Gal Ethanol equiv | 253 | | 1,483,339,000 | Ν | | | | | | | |

| Hawaii distillate, | , resid and coal | import | (125 T BTU) |
|--------------------|------------------|--------|-------------|
|--------------------|------------------|--------|-------------|

COST, THERMO AND CO2 MATRIX AMMONIA NATURAL GAS GASOLINE LPG DIESEL COAL ETHANOL NPUT Price of NH3 **PUT** Price of gas PUT Price of PUT Price of LPG UT Price of diesel PUT Price of coal PUT Price of delivered to site, \$ delivered to site, \$ / gasoline delivered to lelivered to site, \$ / lelivered to site, \$ / delivered to site, \$ / ethanol delivered to per tonne nmbtu site, \$ / gal ite, \$ / gal \$350 \$5.00 \$30.00 \$4.00 \$4.00 \$4.00 \$50 Tonnes NH3 for 21.3 MMBTU gas for 21.3 Gal gasoline for 21.3 Gal diesel for 21.3 Tonnes coal for 21.3 Gal ethanol for 21.3 al LPG for 21.3 MMBTU MMBTU MMBTU ммвти ммвти ммвти ммвти 21 e Fuel Cost (f Fuel Cost (fo B Fuel Cost (for 21.3 as Fuel Cost (for 21.3 G Fuel Cost (for 21.3 el Fuel Cost (for 21.3 al Fuel Cost (for 21.3 .3 mmbtu) - This mmbtu) - This ul - This Scenario ul - This Scenari otu) - This Scenari tu) - This Scenario u) - This Scenari \$35 \$63 \$68 \$936 \$624 \$1,26 kwh from 21.3 mmbtu at kwh from 21.3 mmbtu at kwh from 21.3 mmbtu at wh from 21.3 mmbtu at kwh from 21.3 mmbtu at wh from 21.3 mmbtu at kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 45% efficiency (gas/nh3 45% efficiency (gas/nh3 45% efficiency (gas/nh3 35% efficiency (coal like) 35% efficiency (coal like) 35% efficiency (coal like) 28 220 2800 280 22 220 el cost for power, Fuel cost for power, \$/kwh from NH3 el cost for power for el cost for power, el cost for power, el cost for power, el cost for power, kwh from coal wer, \$/kwh from ga kwh from gasoline wh from LPG wh from diesel kwh from coal \$0.125 \$0.228 \$0.313 \$0.334 \$0.284 \$0.024 \$0.452 MMONIA, NO AMMONIA w/ NATURAL GAS GASOLINE LPG DIESEL COAL ETHANOL ccs HARVEST CO2 per 21.3 CO2 per 21.3 CO2 per 21.3 mmbtu, CO2 per 21.3 mmbtu, CO2 per 21.3 mmbtu, T CO2 per 21.3 mmbtu, T CO2 per 21.3 mmbtu, T CO2 per 21.3 mmbtu, nbtu,only mbtu,only production OT COUNTING OT COUNTING IOT COUNTING OT COUNTING OT COUNTING OT COUNTING CO2 harvest ECYCLE duction, no CCS 0.33 1.93 0.68 1.23 1.65 1.48 1.68 2.42 CASE NOTES HAWAII distillate, resid and coal import (125 T BTU)

Gas price - \$40 per mmbtu

Power - \$350 per mwh (about 80% from coal, resid and fuel oil)

This could be displaced by 6 mmt nh3 (about 7.5 ammonia plants)

About 150 cargo ship deliveries per year.3

Fuel cost for ammonia per year - \$2.0 bb. Fuel cost for power ('free' heat from CHP) - \$125 per

иwн.

Scenario Model

- Inputs are tonnes NH3 and unit costs of fuels.
- **Outputs are parameters** • of the scenario and relative economics.
- Example parameters ٠
- # of ammonia plants •
- # of railcars and ship ٠ cargoes
- MWh of power
- Tonnes of oil, coal, Ing equivalent
- Tonnes of clean water • from NH3 combustion
- · Comparative costs for equivalent BTU's from various fuels



| LNG 2012 Total Trade - 325 BCM | | | | | | | | | | | | _ |
|--|------------------------------------|--|-----------------------|--|--|---|--|---|---|--|--|--|
| мос | DEL RESI | JLTS | | | | COST, T | HERMO AND CO2 | MATRIX | | | | |
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 600,000,000 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | INPUT Price of methanol delivered to site, \$ / tonne | INPUT Price of DME delivered to site, \$ / tonne |
| OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T INI'S BASIS) IN CS. ITERATE D4 TO ACHEVE DESIRED QUANTITY IN D5 | | 0.00 | | \$500 | \$23.00 | \$2.90 | \$2.15 | \$3.20 | \$100 | \$4.00 | \$300 | \$420 |
| MMBTU (or 1000 CF gas equiv) contained in NH3 MMBTU gas required for | 21.32 | 12,790,800,000 | | Tonnes NH3 for 21.3 MMBTU | MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21.3 MMBTU |
| NH3 TCF natural gas required | 32.0 | 19,200,000,000 | | 1.0 NH3 Fuel Cost (for 21.3 | 21.3 Gas Fuel Cost Hor 21.3 | Gasoline Fuel Cost (for 21.3 mmbtu) - This | 234 LPG Fuel Cost (for 21.3 | Diesel Fuel Cost (for 21.3 | Le Coal Fuel Cost (for 21.3 | Ethanol Fuel Cost (for 21.3 mmbtu) - This | 0.982 Methanol Fuel Cost | 0.7 DME Fuel Cost (for |
| for NH3 Tonnes water produced | 2.945-08 | 17.640 | | mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 mmbtu) - This Scenario | Scenario | mmbtu) - This Scenario | mmbtu) - This Scenario | mmbtu) - This Scenario | Scenario | (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario |
| from NH3 # Global ammonia | | 948,000,000 | | \$500 kwh from 21.3 mmbtu at | | \$499 kwh from 21.3 mmbtu at | \$503 kwh from 21.3 mmbtu at | \$499 kwh from 21.3 mmbtu at | \$104 kwh from 21.3 mmbtu at | \$1,012 kwh from 21.3 mmbtu at | \$294 kwh from 21.3 | \$29 kwh from 21.3 |
| Industry # of World Scale NH3 | 6.67E-09 | 4.000 | | 45% efficiency (gas/nh3 like) | ike) | 35% efficiency (coal like) | | kwh from 21.3 mmbtu at 35% efficiency (coal like) | | | mmbtu at 45% efficiency (gas/nh3 | mmbtu at 45% efficiency (gas/nh3 |
| Plants Number of 60,000 cbm | 2,44E-05 | 750.00000 | | 2800 Fuel cost for power, | 2800 Fuel cost for power for | Fuel cost for power, | 2800 Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | 2800 Fuel cost for power, \$/kwh from | 280 Fuel cost for power, |
| vessels Number of 80 tonne | 0.0125 | | | \$/kwh from NH3 \$0.179 | power, \$/kwh from gas \$0.175 | S/kwh from gasoline | \$/kwh from LPG \$0.180 | \$/kwh from diesel | S/kwh from coal | S/kwh from coal | \$/kwh from methanol \$0.105 | \$/kwh from DME |
| railcar deliveries | 0.0125 | 7,500,000 | AMMONIA, NO | AMMONIA w/ | | \$0.227 | | | \$0.047 | \$0.361 | | \$0.10 |
| pipeline MWh from 45% efficient | 2.818+00 | | CCS T CO2 per 21.3 | HARVEST T CO2 per 21.3 | | GASOLINE T CO2 per 21.3 mmbtu, | LPG T CO2 per 21.3 mmbtu, | DIESEL T CO2 per 21.3 mmbtu, NOT COUNTING | | | METHANOL T CO2 per 21.3 | DME T CO2 per 21.3 |
| power plants # of 10 MW plants that | 3.216-05 | 1,686,000,000 | | mmbtu,only production, CO2 harvest | NOT COUNTING LIFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING UFECYCLE | COUNTING LIFECYCLE | COUNTING LIFECYCLE |
| can be run for 1 year, 45% Equivalent # of 6 mtpa | | 19,235.7 | 1.93 | 0.68 | 1.23 | | | 1.68 | 2.42 | 0.33 | 1.80 | 1.8 |
| LNG train (BTU basis) | 6.872-08 | 41.23 | 325 hcm (| * 90 mmtee | /hcm) equi | v to about 3 | NOTES | | | | | |
| Tonnes LNG equivalent | 0.41 | 246,000,000 | 525 benn (| .90 mmtoe | y being equi | v to about 5 | 00 11111 100 | | | | | |
| Metric Tonnes coal equiv | 1.04 | 624,000,000 | This is equ | uivalent to 6 | 00 MM TPA | ammonia (4 | 4 X current a | ammonia inc | lustry) | | | |
| (TOE) | 0.500 | 300,000,000 | | | | | | | | | | |
| Tonnes resid equiv | 0.530 | 318,000,000 | | | | | | | | | | |
| 1.00 in | | 140,400,000,000 | | | | | | | | | | |
| Gal Gasoline equiv | 172 | 103,200,000,000 | | | | | | | | | | |
| Gal Ethanol equiv | 253 | 151,800,000,000 | | | | | | | | | | |
| Price NH3 | \$500 | | | | | | | | | | | |
| Total NH3 cost \$ | \$ 0.179 | 300,000,000,000 | | | | | | | | | | |
| S/kwh from NH3 Price NATURAL GAS | \$23.00 | | | | | | | | | | | |
| | \$23.00 | | | | | | | | | | | |
| Total Natural Gas cost \$ | \$ 0.175 | \$ 293,940,000,000 | | | | | | | | | | |
| Fuel cost for power for power, \$/kwh from gas | \$ 0.175 | | | | | | | | | | | |
| Price GASOLINE | 52.90 | \$ 299,280,000,000 | | | | | | | | | | |
| Total Gasoline cost \$ | | 299,280,000,000 | | | | | | | | | | |
| \$/kwh from gasoline | \$ 0.227 | | | | | | | | | | | |
| Price LPG Total LPG cost \$ | \$2.15 | | | | | | | | | | | |
| Total LPG cost \$ | | \$ 301,860,000,000 | | | | | | | | | | |
| \$/kwh from LPG | \$ 0.180 | | | | | | | | | | | |
| Price DIESEL | \$3.20 | \$ 299,520,000,000 | | | | | | | | | | |
| Total Diesel cost \$ | | \$ 299,520,000,000 | | | | | | | | | | |
| \$/kwh from diesel | \$ 0.227 | | | | | | | | | | | |
| Price COAL | \$100 | | | | | | | | | | | |
| Total Coal cost \$ | | \$ 62,400,000,000 | | | | | | | | | | |
| \$/kwh from coal | \$ 0.047 | | | | | | | | | | | |
| Price ETHANOL | | | | | | | | | | | 1 | |
| | 200 | | | | | | | | | | | |
| Total Ethanol cost \$ | | \$ 607,200,000,000 | | | | | | | | | | |
| | \$ 0.361 \$ 5.50E-07 | \$ 607,200,000,000 | | | | | | | | | | |

Global LNG

LNG Global trade 2012 was equivalent to 600 MM TPA Ammonia

This is equivalent to 4 X current global ammonia business.

This is a proxy of low cost, large scale natural gas available with capability for industrial construction around the world for commercial use.

LNG market does not include:

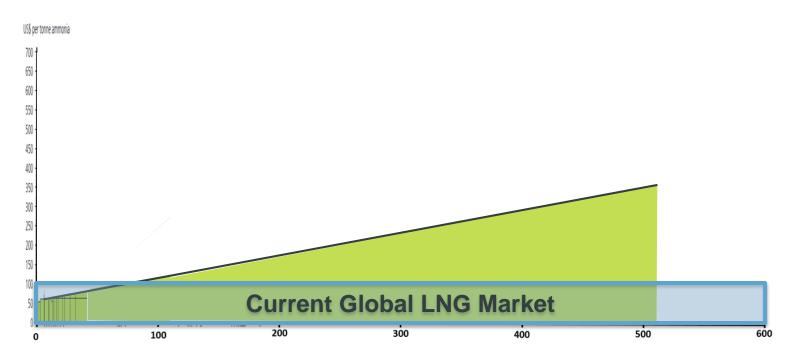
Medium sized resources (< a few TCF)

Difficult access to deep port (e.g., Alaska)

Political barriers (e.g., US shale gas)



What Happens with a Growing Fuels Market?



• There is low cost, commercializable natural gas available for low cost ammonia (especially considering the growing amounts of gas not available for LNG).

| | | | 10% of ALA | SKA LNG pr | oject (10% o | of 60 BB\$ - 1 | 19 mtpa (90 | 0 bcf/yr)) | | | | | | | |
|--|------------------------------------|---|--|---|--|---|--|---|---|---|--|--|--|--|--|
| MODE | RESUL | TS | | | | COST, T | HERMO AND CO2 | MATRIX | | | | | | | |
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | | | | | |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 4,609,757 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | | | | | |
| OPTIONAL USER- DEFINED VARIABLE. INTER VARIABLE NAME N THIS CELL. ENTER (1 T NH3 BASIS) IN CS. TERATE DA TO ACHIEVE DESIRED QUANTITY IN DS | | 0.00 | | \$350 | \$25.00 | \$4.50 | \$3.50 | \$4.00 | \$125 | \$4.50 | | | | | |
| MMBTU contained in NH3 | 21.32 | 98,270,799 | | Tonnes NH3 for 21.3 MMBTU | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | | | | | |
| IMBTU gas required for H3 | 32.0 | 147,512,223 | | 1.0 | 21.3 | 171 | 234 | 156 | 1.0 | 253 | | | | | |
| CF natural gas required or NH3 | 2.94E-08 | 0.14 | | NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 mmbtu) - This Scenario | Gasoline Fuel Cost (for 21.3 mmbtu) - This Scenario | LPG Fuel Cost (for 21.3 mmbtu) - This Scenario | Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario | Coal Fuel Cost (for 21.3 mmbtu) - This Scenario | Ethanol Fuel Cost (for 21.3 mmbtu) - This Scenario | | | | | |
| onnes water produced rom NH3 | 1.585+00 | 7,283,416 | | \$350 \$533 \$774 \$819 \$624 \$130 \$1,189 bit for 71 J method bit for 71 J method | | | | | | | | | | | |
| l Global ammonia ndustry | 6.672-09 | 0.03 | | kwh from 21.3 mmbtu at 45% efficiency (gar/må) 45% efficiency (gar/må) 18ke) | | | | | | | | | | | |
| of World Scale NH3 Plants | 1.258-06 | 5.76 | | 2800 | 2800 | 2200 | 2800 | 2200 | 2200 | 2800 | | | | | |
| lumber of 60,000 cbm ressels | 2.44E-05 | 112 | | Fuel cost for power, \$/kw from NH3 | Fuel cost for power for power, \$/kw from gas | Fuel cost for power, S/kw from gasoline | Fuel cost for power, \$/kw from LPG | Fuel cost for power, \$/kw from diesel | Fuel cost for power, \$/kw from coal | Fuel cost for power, \$/kw from coal | | | | | |
| lumber of 80 tonne ailcar deliveries | 0.0125 | 57,621.96 | | \$0.125 | \$0.190 | \$0.352 | \$0.293 | \$0.284 | \$0.059 | \$0.407 | | | | | |
| of 1 MM TPA NH3 ipeline | 1.005-06 | 4.61 | AMMONIA, NO CCS | AMMONIA w/ HARVEST | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | | | | | |
| 1Wh from 45% efficient ower plants | 2.81E+00 | 12,953,417 | T CO2 per 21.3 mmbtu,only production, no CCS | T CO2 per 21.3 mmbtu,only production, CO2 harvest | T CO2 per 21.3 mmbtu, NOT COUNTING UFECYCLE | T CO2 per 21.3 mmbtu, NOT COUNTING LIFECYCLE | T CO2 per 21.3 mmbtu, NOT COUNTING LIFECYCLE | T CO2 per 21.3 mmbtu, NOT COUNTING LIFECYCLE | T CO2 per 21.3 mmbtu, NOT COUNTING LIFECYCLE | T CO2 per 21.3 mmbtu, NOT COUNTING LIFECYCLE | | | | | |
| of 10 MW plants that an be run for 1 year, 45% | 3.218-05 | 147.79 | 1.93 | | 1.23 | 1.65 | 1.48 | 1.68 | 2.42 | 0.33 | | | | | |
| quivalent # of 6 mtpa NG train (BTU basis) | 6.872-08 | 0.32 | | | | CASE | NOTES | | | | | | | | |
| onnes LNG equivalent | 0.41 | 1,890,000 | | | | | rs of re-injection f ket. The leading c | | | | | | | | |
| letric Tonnes coal equiv | 1.04 | 4,794,147 | pipeline to And | horage and a LNG | export terminal. | In addition to tax | es, revenues and e ing to the point th | employment, the o | development and | monetization of | | | | | |
| onnes oll equivalent OE) | 0.500 | 2,304,878 | increasingly diff | | , Fairbanks and ma | any internal town: | s have very high a | | | | | | | | |
| onnes resid equiv | 0.530 | 2,443,171 | | | | | tain what the LNG | market will be 8- | 10 years from nov | v (after \$60 BB is | | | | | |
| al LPG equiv | 234 | 1,078,683,132 | on the ground) | . This is not a com | nmercial risk. It is | a 'bet the state' r | isk. | | | | | | | | |
| al Gasoline equiv | 172 | 792,878,200 | | | | | ably strong suppor and eventually Asi | | | | | | | | |
| al Ethanol equiv | 253 | 1,166,268,515 | • It doesn't rea | quire mega-invest | ment to prove the | e markets or even | to build the first p | plant. | | | | | | | |
| rice NH3 | \$350 | | | | | | nue, rather than \$ tet is bigger than o | | | | | | | | |
| otal NH3 cost \$ | | \$ 1,613,414,941 | • The market | | | | commodity that is | | | | | | | | |
| uel cost for power, /kwh from NH3 | \$ 0.125 | | | | | | nal AK demand in quired (for power, | | | | | | | | |
| rice NATURAL GAS | \$25.00 | | | red easily for wint | | | | | | 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - 1999 - | | | | | |
| otal Natural Gas cost \$ | | \$ 2,454,695,590 | clean power | gen are very valu | able in this enviro | nment. | lated from finishe | | istrict heating and | d small scale, | | | | | |
| uel cost for power for ower, \$/kwh from gas | \$ 0.190 | | It is not as vi | ulnerable to earth | quakes, sabotage | or high pressure p | pipeline failure as | a gas pipeline. | | | | | | | |
| rice GASOLINE | \$4.50 | | THIS MODEL RE | EFLECTS AMMON | IA PRODUCTION I | EQUIVALENT TO 1 | 0% OF THE PLANN | NED CAPACITY OF | THE LNG/PIPELIN | IE PROJECT. | | | | | |
| otal Gasoline cost \$ | | \$ 3,567,951,899 | This reflects a r | ight-sized scenari | o as an alternative | e to the gas pipelir | ne. | | | | | | | | |
| uel cost for power, /kwh from gasoline | \$ 0.352 | | | | | | lerably more expe But this is actuall | | | | | | | | |
| rice LPG | \$3.50 | | (and it stays in | | ammonia (and me | ethanol/MTG) ind | ustry develops on | | | | | | | | |
| otal LPG cost \$ | | \$ 3,775,390,963 | | | | | on, operation and | logistics to trend | down toward toda | ay's costs (even | | | | | |
| uel cost for power, /kwh from LPG | \$ 0.293 | | as those costs f | fall further). In Ala | aska, higher capex | and operating co | sts will be offset b nsive environment | y very low finding | | | | | | | |
| rice DIESEL | \$4.00 | | | | | , and any other | | | | | | | | | |
| 111 | | | | | | | | | | | | | | | |

Alaska LNG Project

Alaska has massive store of low cost gas from decades of gas re-injection.

There is a \$60-\$70 BB, 6 year project proposed for building a gas pipeline to Anchorage and LNG export to Asia.

10% of the proposed gas would feed 5-6 North Slope ammonia plants.

This can be done in parallel with gas pipeline project, but is much more flexible and quicker payback.



| MOD | EL RESL | ILTS | | % of global ı | | | HERMO AND CO2 | | | | | |
|---|-------------------|---------------------------------------|-------------------------------------|--|--|--|---|--|--|---|-------------------------------------|---------------------------------------|
| USER INPUTS | ALL | ALL VALUES | | AMMONIA | | | | DIESEL | | | | |
| CELLS | EQUIV 1 MT NH3 | CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| REQUIRED INPUT or | 1.00 | 65,600,000 | | INPUT Price of NH3 delivered to site. S | INPUT Price of gas delivered to site, \$ / | INPUT Price of | INPUT Price of LPG delivered to site, \$ / | INPUT Price of diesel delivered to site, \$ / | INPUT Price of coal delivered to site, \$ / | INPUT Price of ethanol delivered to | INPUT Price of methanol | INPUT Price of D delivered to site |
| for your scenario in D4 | 1.00 | - | | delivered to site, \$ per tonne | mmbtu | site, \$ / gal | gal | gal | tonne | site, \$ / gal | delivered to site, \$ / tonne | / tonne |
| OPTIONAL USER- | | | | | | | | | | | | |
| ENTER VARIABLE NAME IN THIS CELL, ENTER (1 T | | 0.00 | | \$350 | \$15.00 | \$3.00 | \$2.00 | \$3.80 | \$50 | \$3.00 | \$200 | \$290 |
| NH3 BASIS) IN CS. ITERATE D4 TO ACHIEVE DESIRED QUANTITY IN D5 | | | | | | | | | | | | |
| MMBTU (or 1000 CF gas | 21.32 | 1,398,460,800 | | | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 | Tonnes coal for 21.3 MMETU | Gal ethanol for 21.3 | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 3 MMBTU |
| equiv) contained in NH3 MMBTU gas required for | 32.0 | 2,099,200,000 | | 14 | 21.1 | | 234 | 154 | IMMETO | 253 | 21.3 MMBT0 0.982 | MMBTU |
| NH3 TCF natural gas required | | | | NH3 Fuel Cost (for 21.3 | Gas Feel Cost (for 21.3 | Gasoline Fuel Cost (for | LPG Fuel Cost (for 21.3 | Diesel Fuel Cost (for 21.3 | Coal Fuel Cost (for 21.3 | Ethanol Fuel Cost (for | Methanol Fuel Cost | OME Fuel Cost (fo |
| for NH3 | 2.942-08 | 1.929 | | mmbtu) - This Scenario | mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario | mmbtu) - This Scenario | mmbtu) - This Scenario | mmbtu) - This Scenario | 21.3 eventsu) - This Scenario | (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - Th Scenario |
| Tonnes water produced from NH3 | 1.588+00 | 103,648,000 | | \$350 kwh from 21.3 mmbtu at | \$320 kwh from 21.3 mmbtu at | \$516 | \$468 kwh from 21.3 mmbtu at | \$593 | \$53 | \$759 kwh from 21.3 mmbtu at | \$196 kwh from 21.3 | swh from 21.3 |
| # Global ammonia industry | 6.672-09 | 0.437 | | | 45% efficiency (gas/nh3 like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | mmbtu at 45% efficiency (gas/nh3 | mmbtu at 45% efficiency (gas/nit |
| I of World Scale NH3 Plants | 1.256-06 | 82.00 | | 2800 | 2900 | 2200 | 2800 | 2200 | 220 | 2800 | 2800 | |
| Number of 60,000 cbm vessels | 2.446-05 | 1,598 | | Fuel cost for power, \$/kwh from NH3 | Fuel cost for power for power, 5/kwh from gas | Fuel cost for power, S/kwh from gasoline | Fuel cost for power, S/kwh from LPG | Fuel cost for power, S/kwh from diesel | Fuel cost for power, S/kwh from coal | Fuel cost for power, S/kwh from coal | Fuel cost for power, \$/kwh from | Fuel cost for pow \$/kwh from DME |
| Number of 80 tonne railcar deliveries | 0.0125 | 820,000 | | \$0.125 | \$0.114 | \$0.235 | \$0.167 | \$0.269 | \$0.024 | \$0.271 | so.070 | \$0. |
| of 1 MM TPA NH3 | 1.005-06 | 65.6 | AMMONIA, NO | AMMONIA w/ | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| pipeline MWh from 45% efficient | 2.818-00 | 184,336,000 | CCS T CO2 per 21.3 mmbhu colo | HARVEST T CO2 per 21.3 | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 | T CO2 per 21.3 |
| power plants | | | production, no CCS | CO2 harvest | UFECYCLE | UFECYCLE | UFECYCLE | UFECYCLE | URECYCLE | UFECYCLE | COUNTING LIFECYCLE | COUNTING LIFECY |
| can be run for 1 year, 45% | 3.211-05 | 2,103.1 | 1.93 | 0.68 | 1.23 | 1.65 | 1.48 | 1.68 | 2.43 | 0.33 | 1.80 | 1 |
| Equivalent # of 6 mtpa LNG train (BTU basis) | 6.872-08 | 4.51 | olahal and | 200 | h la substant à la | | NOTES | and at 10%) | | | | |
| Tonnes LNG equivalent | 0.43 | 26,896,000 | | r power – 2500 tw | | 8.5 Quad at 100%, | about 21 Quad I | heat at 40%} | | | | |
| Metric Tonnes coal equiv | 1.04 | 68,224,000 | Levelling Base | Load for existing r | nuclear. | | | | | | | |
| Tonnes oil equivalent (TOE) | 0.500 | 32,800,000 | Assume typica | I 1 GW nuclear pla be high). Assume | int producing pow | ver at incremental | operating cost of | \$0.02 per kwh (? | Is this a reasonabi | le number, it | | |
| Tonnes resid equiv | 0.530 | 34,768,000 | | this case is that the | | | | | the leferstructure | en for local | | |
| 1.00° in | 234 | 15,350,400,000 | production of a | ammonia power is | in place.) During | peak hours, the a | mmonia power p | roduction (sized to | 25% of baseload | (250 MW)) | | |
| | 172 | 11,283,200,000 | up to 125% of | ent the 750 MW f the original 1 GW. | rom the plant. De | uring peak summe | r months, the am | monia production | could be scaled b | ack to provide | | |
| | | | As infrastructu | ire builds, this cou | ld theoretically gr | ow to 100% amm | onia production fr | rom the nuclear pl | ant. | | | |
| Gal Ethanol equiv | 253 | 16,596,800,000 | The case is 255 | % of current nucle | ar converted via E | lectrogen/FAM, T | his is 625 twh. If i | we assume that 65 | 5% (?. efficiency o | fpower | | |
| Price NH3 | \$350 | | converted to a | immonia BTUs) (41 | 10 twh of this ene | rgy is converted to | o ammonia (21.7 r | mmbtu per tonne) | | 111 | | |
| Total NH3 cost \$ | | 22,960,000,000 | This is 65 MM | tonnes ammonia. | | | | | | | | |
| Fuel cost for power, \$/kwh from NH3 | \$ 0.125 | | | ent of 5000 gpd Ele | | | | | | | | |
| Price NATURAL GAS | \$15.00 | | about \$3BB ca | t that large scale m pex. At \$0.02 per l | kwh and sales prid | ce of \$350/tonne, | the capital will be | paid off within 2- | 3 years. It should | be noted that \$3 | | |
| Total Natural Gas cost 5 | | \$ 20,959,200,000 | BB is a very sm peak capacity | hall investment for by 25%. And at th | upgrading the wo | orids' nuclear flee nonia price, it is a | t to 25% flexibility very profitable in | on diurnal peak s vestment. | having and increa | sing effective | | |
| Fuel cost for power for power, S/kwh from gas | \$ 0.114 | | | associated with th | | | | | able energy. We | will use a | | |
| power, 5/kwh from gas | \$3.00 | | 'theoretical' M | 1HI ammonia Meg CHP/absorptive A | aNinja as a protot | ype (nominally siz | ed as 1.5 MW - 1 | 0 MW, power effic | iency at 45%, add | litional heat | | |
| | | 5 33,849,600,000 | | nes (about \$17 BB | | in assume capex a | r 9900/kw (98 MN | a for 10 Miw mach | intej. Inis scenari | lo requires 2100 | | |
| Total Gasoline cost \$ | | 3 33,849,600,000 | | fficiency, these un | | | | | | | | |
| Fuel cost for power, \$/kwh from gasoline | \$ 0.235 | | | nonia, the total co , the fuel cost for p | | | this scenario is \$2 | 2.8 BB. If we valu | e the heat at \$3/r | nmbtu | | |
| Price LPG | \$2.00 | | | available on stand | | | y installed at the I | highest value sites | (office buildings | highrise | | |
| Total LPG cost \$ | | \$ 30,700,800,000 | dwellings, reta | il, food (refrigerat , medium pressur | tion), light manufa | cturing, banks, ho | | | | | | |
| Fuel cost for power, \$/kwh from LPG | \$ 0.167 | | | | | | | | | | | |
| Price DIESEL | \$3.80 | | 5000 tpd) and | in attributes of thi can initially serve | ammonia fertilize | r markets as well | as dedicated offta | ke to energy. The | energy market ci | an also be started | | |
| Total Diesel cost \$ | | \$ 38,887,680,000 | at small scale (| (e.g., 1.5 MW for h available ammonia | high value CHP or . The real beauty | dedicated uninter is that this marke | ruptible power) an et can grow region | nd it can be supple ally around existin | emented or backe ng nuclear plants. | d up with It can (and will) | | |
| | \$ 0.269 | | grow organica | lly according to pu ir own cost/risk/b | rely economic dri | ivers allowing entr | epreneurs and po | wer customers (a | nd grid managem | ent/regulators) | | |
| Fuel cost for power, | | | to acverop the | | | | | | | | | |
| Fuel cost for power, \$/kwh from diesel | | | | | | | | | | | | |
| Price COAL | 550 | | | | | | | | | | | |
| Price COAL Total Coal cost \$ | 550 | \$ 3,411,200,000 | | | | | | | | | | |
| Price COAL | 550 \$ 0.024 | \$ 3,411,200,000 | | | | | | | | | | |
| Price COAL Total Coal cost \$ | | \$ 3,411,200,000 | | | | | | | | | | |
| Price COAL Total Coal cost 5 Fuel cost for power, S/kwh from coal | S 0.024 | \$ 3,411,200,000 \$ 49,790,400,000 | | | | | | | | | | |
| Price COAL Total Coal cost \$ Fuel cost for power, \$/kwh from coal Price ETHANOL | S 0.024 | | | | | | | | | | | |

Global Nuclear

Nuclear power plants do not follow load (they operate full tilt 24/7). In general, the power overnight is not highly valued and seeks big markets at low prices.

If 25% of global nuclear were to be converted to ammonia at 65% efficiency, this would be equivalent to 65 MM TPA ammonia (about 45% of current global production.)

This requires commercialization of low capital electrolytic production technology.

There are several additional advantages:

Production of fuel for regional grid stabilization (e.g., renewables)

Locally controlled DG/CHP with NH3

Arbitrage of NH3/power by the nuclear plant.



Overview of Sources (for future development)

- Alaska North Slope
- US Southwest/Fracking in general
- Middle East / North Africa (lowest cost ammonia currently, lots of headroom)
- Canada Hydroelectric (10's of GW of low cost power on contract)
- Iceland (practically unlimited geothermal at 3.7 cents/kwh)
- Big Wind (depends on low capex electrolysis tech, allows local grid stabilization)
- Off Peak Nuclear (depends on low capex electrolysis tech, allows local grid stabilization)



Where Are the Markets?



| | DEL RESI | | | 0% 2012 Ne | and a start of a | | | | | | | |
|---|------------------------------------|--|-------------------------------------|--|--|---|--|---|---|--|--|---|
| MO | DEL RESI | | | | | COST, T | HERMO AND CO2 | MATRIX | | | | |
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 11,727,179 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | INPUT Price of methanol delivered to site, \$ / tonne | INPUT Price of DM delivered to site, \$ / tonne |
| OPTIONAL USER DEFINED VARIABLE ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NH3 BASIS) IN CS. TERATE DA TO ACHEVE DESIRED QUANTITY IN OS | | 0.00 | | \$350 | \$12.00 | \$4.00 | \$3.50 | \$4.00 | \$100 | \$4.00 | \$300 | \$420 |
| MMBTU (or 1000 CF gas equiv) contained in NH3 | 21.52 | 250,000,000 | | Tonnes NH3 for 21.3 MMBTU | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21.3 MMBTU |
| MMBTU gas required for NH3 | 32.0 | 375,269,725 | | 14 | | 172 | 234 | 154 | 11 | 253 | 0.982 | 2 0. |
| TCF natural gas required for NH3 | 2.942-08 | 0.345 | | NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario | LPG Fuel Cost (for 21.3 mmbtu) - This Scenario | Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario | Coal Fuel Cost (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario | (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario |
| Tonnes water produced from NH3 # Global ammonia | 1.58E+00 | 18,528,943 | | \$350 kwh from 21.3 mmbtu at | \$256 kwh from 21.3 mmbtu at | \$688 kwh from 21.3 mmbtu at | \$819 kwh from 21.3 mmbtu at | \$624 kwh from 21.3 mmbtu at | \$104 kwh from 21.3 mmbtu at | \$1,012 kwh from 21.3 mmbtu at | \$294 kwh from 21.3 | \$29 kwh from 21.3 |
| a of World Scale NH3 | 6.67E-09 | 0.078 | | 45% efficiency (gas/nh3 like) | 45% efficiency (gas/nh3 like) | 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | 35% efficiency (coal like) | 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | mmbtu at 45% efficiency (gas/nh3 | mmbtu at 45% efficiency (gas/nh3 |
| Plants Number of 60,000 cbm | 1.255-05 | 14.66 | | 2800 Fuel cost for power, S/kwh from NH3 | 2800 Fuel cost for power for | Z200 Fuel cost for power, | 200 Fuel cost for power, \$/kwh from UPG | 2200 Fuel cost for power, S/buth from diesel | Fuel cost for power, S/kwb from coal | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, |
| vessels Number of 80 tonne | 0.0125 | 286 | | S/kwh from NH3 | Fuel cost for power for power, \$/kwh from gas \$0.091 | S/kwh from gasoline | S/kwh from UPG | S/kwh from diesel | \$/kwh from coal | S/kwh from coal | S/kwh from methanol \$0.105 | S/kwh from DME |
| railcar deliveries | 1.005-06 | 146,590 | AMMONIA, NO | AMMONIA w/ | NATURAL GAS | GASOLINE | 50.293 LPG | DIESEL | COAL | 50.361 ETHANOL | S0.105 | DME |
| pipeline MWh from 45% efficient | 2.815+00 | 32,953,373 | CCS T CO2 per 21.3 mmbtu,only | HARVEST T CO2 per 21.3 mmbtu,only production, | T CO2 per 21.3 mmbtu, NOT COUNTING | T CO2 per 21.3 mmbtu, NOT COUNTING | T CO2 per 21.3 mmbtu, NOT COUNTING | T CO2 per 21.3 mmbtu, NOT COUNTING | T CO2 per 21.3 mmbtu, NOT COUNTING | T CO2 per 21.3 mmbtu, NOT COUNTING | T CO2 per 21.3 mmbtu, NOT | T CO2 per 21.3 mmbtu, NOT |
| a of 10 MW plants that can be run for 1 year, 45% | 3.215-05 | 376.0 | production, no CCS | CO2 harvest 0.68 | LIFECYCLE 1.23 | 1.65 | LIFECYCLE 1.48 | URCYCLE 1.68 | 2.42 | 0.33 | COUNTING LIFECYCLE | COUNTING UPECYCL |
| Equivalent # of 6 mtpa LNG train (BTU basis) | 6.872-08 | 0.81 | | 1000 | | CASE | NOTES | | | | | |
| Tonnes LNG equivalent | 0.41 | 4,808,143 | Second Street Street | as and fuel infrast | | | | | | 21.21.21.01 | | |
| Metric Tormes coal equiv | 1.04 | 12,196,266 | | ough pipeline and ually cycle \$10 per | | | | dequate to arbitra | age costs through | the year. | | |
| Tonnes oil equivalent (TOE) | 0.500 | 5,863,589 | | ve sustainably rise | | | | | | | | |
| Tonnes resid equiv | 0.530 | 6,215,405 | DG/CHP measu | | | | | | ity, environmenta | I, cost saving and | | |
| Gal LPG equiv | 234 | 2,744,159,865 | | ent to 14 ammonia alent to about 28 | | | | | s could be supplie | ed by very low | | |
| Gal Gasoline equiv | 172 | 2,017,074,772 | | Canadian hydropo | | | | | | :5.) | | |
| alethanol equiv | 253 | 2,966,976,264 | Ammonia is: | | | | | | | | | |
| Fuel cost for power, | \$350 | | | times of the year | | | | | | | | |
| \$/kwh from NH3 | \$ 0.125 | | utilization o | | | | | | | | | |
| Price NATURAL GAS | \$12.00 | \$ 2,997,466,929 | ammonia a | el and generating re much cheaper a | and distributable | than gas storage. | These strategic r | ocal depots for lar eserves cover risk | ge (strategic rese is and arbitrage fo | rve) storage of or summer | | |
| Fuel cost for power for power, \$/kwh from gas | \$ 0.091 | \$ 2,397,400,523 | This scenario i | winter heating. T s incremental in e | xecution. Starts v | vith small, high va | lue implementati | | | | | |
| power, S/kwh from gas Price GASOUNE | \$4.00 | | | required. With ea arbitrage opportu | | | | | ing to competitive | ness and risk | | |
| Total Gasoline cost \$ | | \$ 8,068,299,090 | | ons that are alread nulti billion S proje | | | | | | multiyear | | |
| Fuel cost for power, \$/kwh from gasoline | \$ 0.313 | | | | | | | | | | | |
| Price LPG | \$3.50 | | Resear Sea Print | | | | | | | | | |
| Total LPG cost \$ | | \$ 9,604,559,527 | Verm | ort Gas | | New York Gas | | | | | | |
| Fuel cost for power, \$/kwh from LPG | \$ 0.293 | | - | MNNNNN | - JW | WANNIN WANN | MM | | | | | |
| Price DIESEL | \$4.00 | | mm | yuluwell | | | | | | | | |
| Total Diesel cost \$ | | \$ 7,317,759,640 | a | | 4 | | | | | | | |
| Fuel cost for power, \$/kwh from diesel | \$ 0.284 | | Resignment (Configuration | na jindar dang | - | gen Transformer Mality | - | | | | | |
| Price COAL | \$100 | \$ 1,219,626,607 | Nite | Ng OF D | | NE LPG | mi | | | | | |
| Total Coal cost \$ | \$ 0.047 | 3 1,219,626,607 | | to whether | - I | 1 March | 1-2 | | | | | |
| \$/kwh from coal Price ETHANOL | \$4.00 | | | Jast . | | LAV . | | | | | | |
| Total Ethanol cost \$ | | \$ 11,867,905,057 | 110724079 | | Tanataa | | and a state of the | | | | | |
| Fuel cost for power, S/kwh from ethanol | \$ 0.361 | | | | | | | | | | | |
| MegaTonnes CO2 saved with NH3 with harvest vs | 5.506-07 | 6 | | | | | | | | | | |
| QAD . | | | | | | | | | | | | |

New England Gas Demand

New England and Mid Atlantic running short of gas and fuel oil for power and heating. Polar vortex put great pressure on power production last winter. Problem is getting worse with shutdown of coal plants.

It is very difficult and expensive to bring more gas into the region. 10% of current gas to the region is equivalent about 12 MM TPA ammonia (about 14 NH3 plants).

Fuel oil prices are routinely about \$4/gal now (about 80% more expensive than ammonia at \$350/tonne).

Ammonia can be used for distributed generation and combined heat/power around the region (energy security, urban deployment, grid stability)



| MOD | DEL RESI | ULTS | | | | COST. T | HERMO AND CO2 | MATRIX | | | | | |
|---|------------------------------------|--|--------------------------------------|--|--|---|--|---|---|--|--|---|--|
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME | |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 5.86E+06 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | INPUT Price of methanol delivered to site, \$ / tonne | INPUT Price of DM delivered to site, \$ / tonne | |
| OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NH3 BASIS) IN CS. ITERATE D4 TO ACHIEVE DESIRED QUANTITY IN D5 | | 0.00 | | \$350 | \$30.00 | \$4.00 | \$4.00 | \$4.00 | \$50 | \$5.00 | \$200 | \$290 | |
| MMBTU (or 1000 CF gas | 21.32 | 124,987,434 | | Tonnes NH3 for 21.3 MMBTU | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21.3 | |
| MMBTU gas required for | 32.0 | 187,616,000 | | 10 | 21.3 | 172 | 234 | 15 | 1.0 | 25 | | 2 0. | |
| TCF natural gas required | 2.945-08 | 0.172 | | NH3 Fuel Cost (for 21.3 | Gas Fuel Cost (for 21.3 | Gasoline Fuel Cost (for 21.3 mmbtu) - This | LPG Fuel Cost (for 21.3 | Diesel Fuel Cost (for 21.3 | Coal Fuel Cost (for 21.3 | Ethanol Fuel Cost (for 21.3 mmbtu) - This | Methanol Fuel Cost (for 21.3 mmbtu) - | DME Fuel Cost (for 21.3 mmbtu) - This | |
| Tonnes water produced | 1.588+00 | 9,263,540 | | saso | ś639 | Scenario \$688 | ś936 | s624 | mmotu) - Inis scenario \$52 | Scenario \$1.265 | This Scenario \$196 | Scenario \$20 | |
| from NH3 # Global ammonia | 6.672-09 | 0.039 | | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at | kwh from 21.3 mmbtu at | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | t kwh from 21.3 mmhtu at 45% | kwh from 21.3 mmbtu at 45% | |
| industry If of World Scale NH3 | 1256.05 | 7.33 | | like) | like) | 35% efficiency (coal like) | like) | 35% efficiency (coal like) | 35% efficiency (coal like) | like) | efficiency (gas/nh3 | efficiency (gas/nh3 | |
| Plants Number of 60.000 cbm | | | | Fuel cost for power. | Fuel cost for power for | Fuel cost for power. | Fuel cost for power. | Fuel cost for power. | Fuel cost for power. | Fuel cost for power, | Fuel cost for power, | Fuel cost for power. | |
| vessels | 2.44E-05 | 143 | | \$/kwh from NH3 | power, S/kwh from gas | \$/kwh from gasoline | \$/kwh from LPG | S/kwh from diesel | \$/kwh from coal | \$/kwh from coal | S/kwh from methanol | \$/kwh from DME | |
| Number of 80 tonne railcar deliveries | 0.0125 | 73,288 | AMMONIA, NO | \$0.125 AMMONIA w/ | \$0.228 | \$0.313 | \$0.334 | \$0.284 | \$0.024 | \$0.452 | \$0.070 | \$0.07 | |
| pipeline | 1.005-06 | 5.9 | AMMONIA, NO CCS T CO2 per 21.3 | AMMONIA w/ HARVEST T CO2 per 21.3 | NATURAL GAS T CO2 per 21.3 mmbtu, | GASOLINE T CO2 per 21.3 mmbtu, | LPG T CO2 per 21.3 mmbtu, | DIESEL T CO2 per 21.3 mmbtu, | COAL T CO2 per 21.3 mmbtu, | ETHANOL T CO2 per 21.3 mmbtu, | METHANOL T CO2 per 21.3 | DME T CO2 per 21.3 | |
| MWh from 45% efficient power plants | 2.818+00 | 16,475,030 | mmbtu,only production, no CCS | mmbtu,only production, CO2 harvest | NOT COUNTING LIFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | mmbtu, NOT COUNTING LIFECYCLE | mmbtu, NOT COUNTING LIFECYCLI | |
| # of 10 MW plants that can be run for 1 year, 45% | 3.218-05 | 188.0 | 1.93 | 0.68 | 1.23 | 1.65 | 1.48 | 1.68 | 2.42 | 0.33 | 3 1.80 | 1.8 | |
| Equivalent # of 6 mtpa LNG train (BTU basis) | 6.87E-08 | 0.40 | | | | CASE | NOTES | | | | | | |
| Tonnes LNG equivalent | 0.41 | 2,403,830 | HAWAII d | istillate, res | id and coal | import (125 | T BTU) | | | | | | |
| Metric Tonnes coal equiv | 1.04 | 6,097,520 | | | | | | | | | | | |
| Tonnes oil equivalent (TOE) | 0.500 | 2,931,500 | Gas price - | \$40 per mmb | tu | | | | | | | | |
| Tonnes resid equiv | 0.530 | 3,107,390 | | 50 per mwh (a | | | | | | | | | |
| Gal LPG equiv | 234 | 1.371.942.000 | | be displaced b | | | mmonia plant | s) | | | | | |
| Gal Gasoline equiv | 172 | 1,008,436,000 | | cargo ship de | | | | | | | | | |
| Gal Ethanol equiv | 253 | 1,483,339,000 | Fuel cost fo | or ammonia p | er year - \$2.0 | bb. Fuel cost | for power ('fi | ree' heat fron | n CHP) - \$12 5 | per | | | |
| | 255 | 1,483,339,000 | | or gas per yea | - \$37 | bb. Euel cost | for nower ('fr | ree' heat fron | o CHP) - \$228 | ner MWH | | | |
| Price NH3 | \$350 | | | or diesel per y | | | | ree' heat from | | | | | |
| Total NH3 cost \$ | | 2,052,050,000 | MWH. | , alessiper , | | | ioi ponei (ii | | , | | | | |
| Fuel cost for power, \$/kwh from NH3 | \$ 0.125 | | Fuel cost fo | or coal per yea | ar - \$0.3 l | ob. Fuel cost f | or power ('fre | ee' heat from | CHP) - \$30 |) per MWH. | | | |
| Price NATURAL GAS | \$30.00 | | | | | | | | | | | | |
| Total Natural Gas cost \$ | | \$ 3,746,457,000 | Fuel price r | not the whole | story. | | | | | | | | |
| Fuel cost for power for power, \$/kwh from gas | \$ 0.228 | | | nuch easier to | | | - | | | | | | |
| Price GASOLINE | \$4.00 | | | nuch cleaner | | | | | | | | | |
| Total Gasoline cost \$ | | \$ 4,033,744,000 | | | | | | cales betwee Coal and gas (| | 50 M. At a | | | |
| Fuel cost for power, | \$ 0.313 | | | | | | | tes CHP (hea | | ve AC, hot | | | |
| S/kwh from gasoline Price LPG | \$4.00 | | | | | | | g fuels (perha | | | | | |
| Total LPG cost \$ | | \$ 5,487,768,000 | electricity. | | | | | | | | | | |
| Fuel cost for power, | \$ 0.334 | J, 467, 706,000 | | | | | | round the wo | | | | | |
| \$/kwh from LPG | | | higher price | | onstieu. That | existing dem | and for fuel c | oil, LPG, LNG I | ias establishe | a much | | | |
| Price DIESEL | \$4.00 | | | | | | | | | | | | |
| Total Diesel cost \$ | | \$ 3,658,512,000 | | | | | | | | | | | |
| Fuel cost for power, \$/kwh from diesel | \$ 0.284 | | | | | | | | | | | | |
| Price COAL | \$50 | | | | | | | | | | | | |
| Total Coal cost \$ | | \$ 304,876,000 | | | | | | | | | | | |
| Fuel cost for power, \$/kwh from coal | \$ 0.024 | | | | | | | | | | | | |
| Price ETHANOL | \$5.00 | | | | | | | | | | | | |
| Total Ethanol cost \$ | | \$ 7,416,695,000 | | | | | | | | | | | |
| Fuel cost for power, S/kwh from ethanol | \$ 0.452 | | | | | | | | | | | | |
| S/kwh from ethanol MegaTonnes CO2 saved | | | | | | | | | | | | | |

Hawaii resid/distillate

Most of Hawaii's electricity is generated from heavy hydrocarbons. This is expensive (HI power more than 3X cost of mainland) and environmentally destructive, 35-40 cents/kwh). Hawaii is working very hard to reduce hydrocarbon reliance (small scale LNG, renewables energy efficiency).

There is great scope for this since power is so expensive. But the cheapest way is through ammonia.

Displacing all of HI resid, fuel oil and coal about equivalent to 6 MMTPA NH3 (about 7 plants or 140 cargo ship deliveries.) Ammonia at \$350/tonne has a fuel cost of 13 cents / kwh (not counting credit for CHP from ammonia diesel gen sets).



| | EL RESU | | | | | COST, T | HERMO AND CO2 | MATRIX | | | | |
|--|---|---|--|--|--|---|---|---|---|--|--|--|
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 1,600,000 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | INPUT Price of methanol delivered to site, \$ / tonne | INPUT Price of DN delivered to site, : / tonne |
| OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T INT3 BASIS) IN CS. ITERATE DA TO ACHIEVE DESIRED QUANTITY IN DS | | 0.00 | | \$500 | \$23.00 | \$2.90 | \$2.15 | \$3.20 | \$100 | \$4.00 | \$300 | \$420 |
| MMBTU (or 1000 CF gas equiv) contained in NH3 | 21.32 | 34,108,800 | | Tonnes NH3 for 21.3 MMBTU | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21. MMBTU |
| MMBTU gas required for NH3 | 32.0 | 51,200,000 | | 14 | 21.3 | 172 | 234 | 154 | 1.0 | 253 | 0.982 | . 0 |
| TCF natural gas required for NH3 | 2.942-08 | 0.047 | | NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 mmbtu) - This Scenario | Gasoline Fuel Cost (for 21.3 mmbtu) - This | LPG Fuel Cast (for 21.3 mmbtu) - This Scenario | Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario | Coal Fuel Cost (for 21.3 mmbtu) - This Scenario | Ethanol Fuel Cost (for 21.3 mmbtu) - This | Methanol Fuel Cost (for 21.3 mmbtu) - | DME Fuel Cost (for 21.3 mmbtu) - This |
| Tonnes water produced from NH3 | 1.588+00 | 2,528,000 | | \$500 | \$490 | Scenario \$499 | \$503 | \$499 | \$104 | Scenario \$1,012 | This Scenario \$294 | Scenario \$25 |
| # Global ammonia industry | 6.678-09 | 0.011 | | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% | kwh from 21.3 mmbtu at 45% |
| # of World Scale NH3 | 1.258-06 | 2.00000 | | like) 2800 | like) 2800 | 2200 | like) 2800 | 2200 | 2200 | 8ke) 2800 | efficiency (gas/nh3 2800 | efficiency (gas/nh3 |
| Number of 60,000 cbm | 2.446-05 | 39 | | Fuel cost for power, | Fuel cost for power for | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, | Fuel cost for power, S/kwh from | Fuel cost for power, |
| vessels Number of 80 tonne | 0.0125 | 20.000 | | \$/kwh from NH3 \$0.179 | power, \$/kwh from gas \$0.175 | \$/kwh from gasoline \$0.227 | S/kwh from LPG | 5/kwh from diesel \$0.227 | \$/kwh from coal \$0.047 | \$/kwh from coal \$0.361 | methanol \$0.105 | S/kwh from DME |
| railcar deliveries | 1.006-06 | 1.6 | AMMONIA, NO | AMMONIA w/ | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| pipeline MWh from 45% efficient | | | CCS T CO2 per 21.3 | HARVEST T CO2 per 21.3 | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 | T CO2 per 21.3 |
| power plants | 2.816+00 | 4,496,000 | mmbtu,only production, no CCS | mmbtu,only production, CO2 harvest | UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING LIFECYCLE | LIFECYCLE | NOT COUNTING LIFECYCLE | COUNTING LIFECYCLE | COUNTING LIFECYCL |
| can be run for 1 year, 45% | 3.218-05 | 51.295 | 1.93 | 0.68 | 1.23 | 1.65 | 1.48 | 1.68 | 2.42 | 0.33 | 1.80 | 1.8 |
| LNG train (BTU basis) | 6.872-08 | 0.11 | 4 MAA AA | is about 140 to | M rupple = 4000 | | NOTES | | | | | |
| Tonnes LNG equivalent | 0.41 | 656,000 | To generate | 4 mm MWh at | | 6 equivalent to 1. | 6 MM Tonnes p | per year of amn | nonia (taking no | account of | | |
| Metric Tonnes coal equiv | 1.04 | 1,664,000 | CHP) Fuel cost for | power (no cred | lit for CHP and | flexibility in disp | atch) at \$500/t | tonne is \$180 p | er MWh | | | |
| Tonnes oil equivalent (TOE) | 0.500 | 800,000 | This can be o | delivered by 40 | cargo loads | | | | | | | |
| Tonnes resid equiv | 0.530 | 848,000 | Server and Manufacture | | | deployed in va | | | | | | |
| Gal LPG equiv | 234 | 374,400,000 | On 2 of the r | najor islands, el | ectricity rates a | are over 40 cent | s/kwh. Even or | n Oahu, they ar | e 30. | | | |
| Gal Gasoline equiv | 172 | 275,200,000 | | | | | | | | | | |
| Gal Ethanol equiv | 253 | 404,800,000 | | hibit 6: Impact of Enge | m Efficiency Distribu | ted Generation, and R | enewable Enermy | | | | [| |
| Price NH3 | \$500 | | - | | Adde | d Cumulativ | e Total bu 202 | 0 | | | | |
| Total NH3 cost \$ | | 800,000,000 | EnergyE | fliciency Savings | twh/year) (MWh/y | rear) (MWh/yea | | | | | | |
| Fuel cost for power, \$/kwh from NH3 | \$ 0.179 | | Distribut | ed Generation | 189,563 40 | 1,572 76 | 2,466 952,0 1,228 2,595,0 | | | | | |
| Price NATURAL GAS | \$23.00 | | Source: PU Report for | C Docket No. 2010-0037; Pi | JC Report to the 2014 Legis | | 0,089 5,897,6 | itus Abou | at 440 MW | | | |
| Total Natural Gas cost \$ | | \$ 783,840,000 | Office Ren 2013; Haw | ewable Energy Projects Dire all Public Utilities Commissio | ctory; 2023 integrated Resi on Document Management | eport for the year ending D surce Planning Report, Hawt System (DMS); Regulatory a | ian Electric Companies, Au gency postings and notices | abou ICF | it 4 mm MWh | | | |
| Fuel cost for power for | \$ 0.175 | | Aralysis. | | | | | | | | | |
| power, \$/kwh from gas | \$2.90 | | will likely be | producing 952,029 M | Wh/year in customer | l electricity demand by generated electricity a | nd another 2,595,612 | | | | | |
| Price GASOL PH | | | MWh/year i | a utility scale second | ele generation. The tot | al impact of these tree | | | | | | |
| Price GASOLINE | | | annual dem | | | in by a total of 3,780,0 | | n | | | | |
| Total Gasoline cost \$ | | \$ 798,080,000 | annual dem 2013-2020. | and for fossil-fuel-base | ed electricity generatio | on by a total of 3,780,0 | | n | | | | |
| Total Gasoline cost \$ Fuel cost for power, \$/kwh from gasoline | \$ 0.227 | 5 798,080,000 | annual dem 2013-2020. | | ed electricity generatio | on by a total of 3,780,0 | | n | | | | |
| Total Gasoline cost \$ Fuel cost for power, \$/kwh from gasoline Price LPG | | | 2013-2020. Averag | and for fossil-fuel-base | ed electricity generation | on by a total of 3,780,0 | | n | | | | |
| Total Gasoline cost \$ Fuel cost for power, \$/kwh from gasoline Price LPG Total LPG cost \$ | \$ 0.227 \$2.15 | 5 798,080,000 S 804,960,000 | 2013-2020. Averag | and for fossil-fuel-base e Electric Rate I | Ad electricity generation | in by a total of 3,780,0 y: 2011 | 89 <u>MWb</u> /year between | | | | | |
| Total Gasoline cost \$ Fuel cost for power, \$/kwh from gasoline Price LPG | \$ 0.227 | | annual dem 2013-2020. Averag | and for fossil-fuel-base e Electric Rate I Cents/kWh | ed electricity generation | on by a total of 3,780,0 y: 2011 40.2 | 42.0 | n | | | | |
| Total Gasoline cost \$ Fuel cost for power, \$/kwh from gasoline Price LPG Total LPG cost \$ Fuel cost for power, | \$ 0.227 \$2.15 | | annual dem 2013-2020. Averag | e Electric Rate Cents/kWh | St electricity generation | on by a total of 3,780,0 y: 2011 40.2 | 42.0 17.2 | n | | | | |
| Tetal Gasoline cost 5 Feel cost for power, Sythant from pasoline Price LPG Tetal LPG cost 5 Feel cost for power, Sythant from LPG Price DESEL Tetal Desel cost 5 | \$ 0.227 \$2.15 \$ 0.180 | | annual dem 2013-2020. Averag | e Electric Rate Cents/kWh | Ad electricity generation | en by a total of 3,780,0 y: 2011 40.2 14.4 | 42.0 | n | | | | |
| Total Gasoline cost \$ Fuel cost for power, \$/kwh from gasoline Price LPG Total LPG cost \$ Fuel cost for power, \$/kwh from LPG Price DIESEL | \$ 0.227 \$2.15 \$ 0.180 | \$ 804,960,000 | annual dem 2013-2020. Averag | e Electric Rate Cents/KWh asse Rates Energy 21.2 | St electricity generation | en by a total of 3,780,0 y: 2011 40.2 14.4 | 42.0 17.2 | n | | | | |
| Tetal Gasoline cost S Fuel cost for power, Shahn from gasoline Price UPG Total LPG cost S Fuel cost for power, Shahn from LPG Price DESLL Tetal Diesel cost S Fuel cost for power, Fuel cost for power | \$ 0.227 \$2.15 \$ 0.180 \$ 3.20 | \$ 804,960,000 | annual dem 2013-2020. Averag | e Electric Rate Cents/KWh ase Rates Energy Costs HECO Godiuj | A electricity generation | 40.2 14.4 20.8 HELCO (Hawilli) | 42.0 17.2 24.0 KiUC Keuai) | n | | | | |
| Tetal Gasoline cost \$ Feel cost for prover, Shash from pasoline Price LPG Tetal LPG cost \$ Tetal CPG cost \$ Price DISSL Tetal Dissel cost \$ Tetal Dissel cost \$ Tetal Dissel cost \$ File cost for prover, \$hash from direct | \$ 0.227 \$2.15 \$ 0.180 \$3.20 \$ 0.227 | \$ 804,960,000 | annual dem 2013-2020. Averag | e Electric Rate Cents/KWN ase Rates 7.4 Energy 21.7 Costs 21.7 HECCO Ochu) 200000 7.200 | d electricity generation | 40.2 14.4 20.8 HELCO (Hawilli) | 42.0 17.2 24.8 KIUC KIUC 50 50 50 50 | n | | | | |
| Tetal Gazoline cont \$ Feel cost for power, \$7Nah from gazoline Price LPG Tetal LPG cost \$ Tetal CPG cost \$ Price DISSE. Price DISSE Tetal Dissel cost \$ Feel cost for power, \$7Nah from dissel Price COAL | \$ 0.227 \$2.15 \$ 0.180 \$3.20 \$ 0.227 | 5 804,860,000 5 798,720,000 | annual dem 2013-2020. <u>Averag</u> B | e Electric Rate Cents/KWh ase Rates 7.4 Energy 21.7 Energy 21.7 HECCO Costu 22000 1000hu | 35.5 11.0 4.5 MECO (Maru) 4.30 1.41 | 40.2 14.4 25.8 HELCO (flavali) | 42.0 17.2 24.8 KIUC Keuai) | n | | | | |
| Tetal Gasoline cost 5 Feet cost for power, Shah from gasoline Feet Cost for power, Shah from UG Feet cost for power, Shah from UG Feet cost for power, Shah from disel Feet cost for power, Shah from disel Feet cost are power, Shah from disel Feet cost are power, Shah from disel Feet cost are power, Feet | \$ 0.227 \$2.15 \$ 0.180 \$ 1.27 \$ 0.227 \$100 | 5 804,860,000 5 798,720,000 | Contraments Contraments Exercision Exercision Contraments Exercisi | e Electric Rate Cents/KWh ase Rates 7.4 Energy 21.7 Energy 21.7 HECCO Costu 22000 1000hu | 35.5 11.0 24.5 MECO (Mau) 6.300 4.30 720 720 | 40.2 14.4 25.8 HELCO (flavnili) 40.2 14.4 25.8 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.2 HELCO (flavnil | 42.0 17.2 24.8 KUCC KUCC 500 100 100 100 100 | | | | | |
| Tetal Gasoline cost 5 Feed cost for power, Shack from gasoline Tetal LPG cost 5 Feed Cost 6 Feed Cost | \$ 0.227 \$2.15 \$ 0.180 \$ 3.30 \$ 0.227 \$ 100 \$ 0.047 | 5 804,860,000 5 798,720,000 | Contraments Contraments Exercision Exercision Contraments Exercisi | e Electric Rate Cents/KWh ase Rates 7.4 Energy 21.7 Energy 21.7 HECCO Costu 22000 1000hu | 35.5 11.0 24.5 MECO (Mau) 6.300 4.30 720 720 | 40.2 14.4 25.8 HELCO (flavnili) 40.2 14.4 25.8 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.2 HELCO (flavnil | 42.0 17.2 24.8 KUCC KUCC 500 100 100 100 100 | n | | | | |
| Tetal Gaudine cost S Feed cost for power, Shade from gaudine Feed UPG cost S Feed UPG cost S Feed Cost Georgen, Shade from UPG Feed DESEL Tetal Cost Georgen, Shade from desel Feed cost s | \$ 0.227 \$2.15 \$ 0.180 \$ 3.30 \$ 0.227 \$ 100 \$ 0.047 | 5 804,360,000 5 798,720,000 5 186,400,000 | Contraments Contraments Exercision Exercision Contraments Exercisi | e Electric Rate Cents/KWh ase Rates 7.4 Energy 21.7 Energy 21.7 HECCO Costu 22000 1000hu | 35.5 11.0 24.5 MECO (Mau) 6.300 4.30 720 720 | 40.2 14.4 25.8 HELCO (flavnili) 40.2 14.4 25.8 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.00 HELCO (flavnili) 40.2 HELCO (flavnil | 42.0 17.2 24.8 KUCC KUCC 500 100 100 100 100 | | | | | |

Hawaii Alternatives Goals

Hawaii's goal is to have capacity for 4 MM MWh from Solar, wind and efficiency by 2020.

This is equivalent to 1.6 MM TPA ammonia. And likely much more expensive.



| | | 1/8 of m | nidwest pro | pane dema | nd and IL an | nual purcha | se of NH3 (| 1 MM tonne | es) | | | | | |
|---|------------------------------------|--|----------------------------------|--|--|---|--|---|---|--|--|--|--|--|
| MOD | EL RESU | JLTS | | | | COST, T | HERMO AND CO2 | MATRIX | | | | | | |
| USER INPUTS ALLOWED IN GREEN CELLS | ALL VALUES EQUIV 1 MT NH3 | ALL VALUES CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME | | |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 1,000,000 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | INPUT Price of methanol delivered to site, \$ / tonne | INPUT Price of DME delivered to site, \$ / tonne | | |
| OPTIONAL USER- DEFINED VARIABLE ENTER VARIABLE NAME IN THIS CELL ENTER (1 T INIS BASIS) IN CS. ITERATE DA TO ACHIEVE DESIRED QUANTITY IN DS | | 0.00 | | \$350 | \$12.00 | \$4.00 | \$3.50 | \$4.00 | \$100 | \$4.00 | \$300 | \$420 | | |
| MMBTU (or 1000 CF gas equiv) contained in NH3 | 21.32 | 21,318,000 | | Tonnes NH3 for 21.3 MMBTU | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21.3 MMBTU | | |
| MMBTU gas required for NH3 | 32.0 | 32,000,000 | | 14 | 21.1 | 172 | 23 | 154 | 1.0 | 251 | 0.982 | 0.71 | | |
| TCF natural gas required for NH3 | 2.948-08 | 0.029 | | NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario | LPG Fuel Cost (for 21.3 mmbtu) - This Scenario | Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario | Coal Fuel Cost (for 21.3 mmbtu) - This Scenario | Ethanol Fuel Cost (for 21.3 mmbtu) - This Scenario | (for 21.3 mmbtu) - This Scenario | 21.3 mmbtu) - This Scenario | | |
| Tonnes water produced from NH3 E Global ammonia | 1.588+00 | 1,580,000 | | \$350 kwh from 21.3 mmbtu at | | \$688 | \$819 kwh from 21.3 mmbtu at | \$624 | \$104 kwh from 21.3 mmbtu at | \$1,012 kwh from 21.3 mmbtu at | \$294 kwh from 21.3 | \$298 kwh from 21.3 | | |
| # Grobal ammonia industry # of World Scale NH3 | 6.678-09 | 0.007 | | 45% efficiency (gas/nh3 like) | 45% efficiency (gas/nh3 like) | 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | 35% efficiency (coal like) | 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | mmbtu at 45% efficiency (gas/nh3 | mmbtu at 45% efficiency (gas/nh3 | | |
| Plants Number of 60,000 cbm | 1258-06 | 1.25 | | 2800 | 280 | 2200 | 2800 | 2200 | 2200 | 2800 | Fuel cost for power, | 2800 | | |
| Number of 60,000 cbm vessels Number of 80 tonne | 2,448-05 | 24 | | Fuel cost for power, \$/kwh from NH3 | Fuel cost for power for power, S/kwh from gas | Fuel cost for power, 5/kwh from gasoline | Fuel cost for power, \$/kwh from LPG | Fuel cost for power, \$/kwh from diesel | Fuel cost for power, \$/kwh from coal | Fuel cost for power, \$/kwh from coal | \$/kwh from methanol | Fuel cost for power, \$/kwh from DME | | |
| Number of 80 tonne railcar deliveries | 0.0125 | 12,500 | AMMONIA, NO | \$0.125 AMMONIA w/ | \$0.091 | \$0.313 | \$0.293 | \$0.284 | \$0.047 | \$0.361 | \$0.105 | \$0.107 | | |
| pipeline MWh from 45% efficient | 1.005-06 | 1.0 | CCS T CO2 per 21.3 | HARVEST T CO2 per 21.3 | NATURAL GAS | GASOLINE T CO2 per 21.3 mmbtu, | LPG T CO2 per 21.3 mmbtu, | DIESEL T CO2 per 21.3 mmbtu, | COAL T CO2 per 21.3 mmbtu, | ETHANOL T CO2 per 21.3 mmbtu, | METHANOL T CO2 per 21.3 | DME T CO2 per 21.3 | | |
| power plants | 3.215-05 | 2,810,000 | mmbtu,only production, no CCS | mmbtu,only production, CO2 harvest | UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING LIFECYCLE | NOT COUNTING LIFECYCLE | UFECYCLE | COUNTING LIFECYCLE | COUNTING LIFECYCLE | | |
| can be run for 1 year, 45% | 3.21E-05 | 32.1 | 1.93 | 0.68 | 1.23 | 1.65 | 1.48 NOTES | 1.68 | 2.42 | 0.33 | 1.80 | 1.80 | | |
| Equivalent # of 6 mtpa LNG train (BTU basis) Tonnes LNG equivalent | 0.41 | 410,000 | Midwest | ertilizer He | eat and Elect | 2.0 | NOTES | | | | | | | |
| Metric Tonnes coal emain | 100 | 1,040,000 | | | | | | | | | | | | |
| Tonnes oil equivalent | 0.500 | 500,000 | | | | v of LPG for hea propane from : | | | | | | | | |
| (TOE) Tonnes resid equiv | 0.530 | 530,000 | | | | or drying extra | | | | | | | | |
| Gal LPG equiv | 234 | 234.000.000 | Prices rose to | o \$4-5 per gallo | n (normally arc | ound \$2). And a | lot of people g | ot really cold a | nd mad. | | | | | |
| Gal Gasoline equiv | 172 | 172.000.000 | | | | CAN L. | | | | 14 | | | | |
| Gal Ethanol equiv | 253 | 253,000,000 | ammonia fe | rtilizer). If 12.5 | % of LPG dema | % of Midwest p nd were stored | at ammonia fa | cilities at the en | d of harvesting | and the start | 1 | I | | |
| Price NH3 | \$350 | | | | | ng low because g the costs and | | | | | | | | |
| Total NH3 cost \$ | | 350,000,000 | | | | The total cost IM and at \$4/ga | | | | | | | | |
| Fuel cost for power, S/kwh from NH3 | \$ 0.125 | | | | of risk managen | | | | | | | | | |
| Price NATURAL GAS | \$12.00 | | | | | s with Sturman | | | | | | | | |
| Total Natural Gas cost \$ | | \$ 255,600,000 | units are also | o ideally suited | | conditioned pov | | | | | | | | |
| Fuel cost for power for power, \$/kwh from gas | \$ 0.091 | | importantly, | crop drying. | | | | | | | | | | |
| Price GASOLINE | \$4.00 | | | | | al infrastructur G infrastructure | | | | | | | | |
| Total Gasoline cost \$ | | \$ 688,000,000 | | | | will be happy to | | | | | | | | |
| Fuel cost for power, S/kwh from gasoline | \$ 0.313 | | | | | | | | | | | | | |
| Price LPG | \$3.50 | | | | | | | | | | | | | |
| Total LPG cost \$ | | \$ 819,000,000 | | | | | | | | | | | | |
| Fuel cost for power, \$/kwh from LPG | \$ 0.293 | | | | | | | | | | | | | |
| Price DIESEL | \$4.00 | | | | | | | | | | | | | |
| Total Diesel cost \$ | | \$ 624,000,000 | | | | | | | | | | | | |
| Fuel cost for power, \$/kwh from diesel | \$ 0.284 | | | | | | | | | | | | | |
| Price COAL | \$100 | | | | | | | | | | | | | |
| Total Coal cost S | | \$ 104,000,000 | | | | | | | | | | | | |
| Fuel cost for power, S/kwh from coal | \$ 0.047 | | | | | | | | | | | | | |
| Price ETHANOL | \$4.00 | | | | | | | | | | | | | |
| Total Ethanol cost \$ | | \$ 1,012,000,000 | | | | | | | | | | | | |
| Fuel cost for power, S/kwh from ethanol | \$ 0.361 | | | | | | | | | | | | | |

MidWest LPG Demand

The Midwestern states ran dangerously low of LPG for heat and farm use this winter with emergency measures required. Even with growing availability of propane from shale oil and gas, the infrastructure for delivery and storage of propane was strained by high demand for drying extra wet crops followed by record cold.

Prices rose to \$4-5 per gallon (normally around \$2). And a lot of people got really cold and mad.

1/8 of MidWest LPG demand is 1 MM TPA NH3. Even at \$500 per tonne, ammonia BTUs are 20% cheaper than \$4/gal LPG.

If ammonia diesel gens were sited on farms and neighborhoods, they would produce wellconditioned power for local use and utility offtake at 45% efficiency. The units are also ideally suited for CHP (total efficiency up to 75% or so) which can be used for district heating and, very importantly, crop drying.

One other huge advantage is countercyclical infrastructure use. The ammonia infrastructure is weighted toward winter and spring (for planting) and the LPG infrastructure is weighted toward summer and fall (for crop drying and winter heating). The ammonia producers might be happy to have profitable smoothing of their storage and distribution.



| 1000 | EL RESU | 175 | | | | I Diesel (700 | HERMO AND CO2 | MATRIX | | | | |
|--|-------------------|--|----------------------------------|--|--|--|---|--|--|---|--|---|
| USER INPUTS | | ALL VALUES CORRESPOND TO CASE PARAMETERS | | | | | | | | | | |
| ALLOWED IN GREEN CELLS | EQUIV 1 MT NH3 | CORRESPOND TO CASE PARAMETERS | | AMMONIA | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME |
| REQUIRED INPUT or | 1.00 | 4,487,179 | | INPUT Price of NH3 delivered to site, \$ | INPUT Price of gas delivered to site, \$ / | INPUT Price of gasoline delivered to | INPUT Price of LPG delivered to site, \$ / | INPUT Price of diesel delivered to site, \$ / | INPUT Price of coal delivered to site, \$ / | INPUT Price of ethanol delivered to | INPUT Price of methanol | INPUT Price of DME delivered to site, \$ |
| for your scenario in D4 | 1.00 | 4,467,175 | | per tonne | mmbtu | site, \$ / gal | gal | gal | tonne | site, \$ / gal | methanol delivered to site, \$ / tonne | / tonne |
| OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NH3 BASIS) IN CS. ITERATE DA TO ACHEVE DESIRED QUANTITY IN DS | | 0.00 | | \$500 | \$10.00 | \$4.00 | \$4.00 | \$4.00 | \$100 | \$4.00 | \$300 | \$420 |
| MMBTU (or 1000 CF gas | 21.32 | 95,657,692 | | Tonnes NH3 for 21.3 MMBTU | MMBTU gas for 21.3 | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21.3 MMBTU |
| MMBTU gas required for | 32.0 | 143,589,744 | | 1.0 | 21.1 | | | 15 | | | 0.982 | 0.71 |
| NH3 TCF natural gas required | 1000 | 0.132 | | NH3 Fuel Cost (for 21.3 | Gas Fuel Cost (for 21.3 | Gasoline Fuel Cost (for | LPG Fuel Cost (for 21.3 | Diesel Fuel Cost (for 21.3 | Coal Fuel Cost (for 21.3 | Ethanol Fuel Cost (for | Methanol Fuel Cost | DME Fuel Cost (for |
| for NH3 | | | | mmbtu) - This Scenario | minolog - mis scenario | Scenario | mmbtu) - This Scenario | mmbtu) - This Scenario | mmbtu) - This Scenario | 21.3 mmotu) - This Scenario | (for 21.3 mmotu) - This Scenario | 21.3 mmotu) - This Scenario |
| from NH3 | 1.588+00 | 7,089,744 | | \$500 kwb from 21.3 mmbtu at | \$213 kwh from 21.3 mmbtu at | \$688 | \$936 kwh from 21.3 mmbtu at | \$624 | \$104 | \$1,012 kwh from 21.3 mmbtu at | \$294 kmb from 21.3 | \$298 kwh from 21.3 |
| II Global ammonia industry | 6.672-09 | 0.030 | | kwn from 21.3 mmbtu at 45% efficiency (gas/nh3 like) | 45% efficiency (gas/nh3 like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | 45% efficiency (gas/nh3 like) | nmbtu at 45% efficiency (gas/nh3 | nmbtu at 45% efficiency (gas/nh3 |
| # of World Scale NH3 Plants | 1.258-06 | 5.60897 | | 2800 | 2800 | 2200 | 2800 | 2200 | 2200 | 280 | 2800 | 280 |
| Number of 60,000 cbm | 2.446-05 | 109 | | Fuel cost for power, \$/kwh from NH3 | Fuel cost for power for power, S/kwh from ray | Fuel cost for power, \$/kwh from pasoline | Fuel cost for power, \$/kwh from LPG | Fuel cost for power, \$70wh from diesel | Fuel cost for power, | Fuel cost for power, S/kwh from coal | Fuel cost for power, S/kwh from | Fuel cost for power, S/kwh from DME |
| Number of 80 tonne | 0.0125 | 56,090 | | \$0.179 | power, 5/kwn trom gas | \$0.313 | \$0.334 | \$0.284 | \$0.047 | \$0.361 | methanol \$0.105 | \$0.107 |
| railcar deliveries | | | AMMONIA, NO | AMMONIA w/ | | | | | | | | |
| pipeline | 1.005-06 | 4.5 | CCS T CO2 per 21.3 | HARVEST T CO2 per 21.3 | NATURAL GAS T CO2 per 21.3 mmbtu, | GASOLINE T CO2 per 21.3 mmbtu, | LPG T CO2 per 21.3 mmbtu, | DIESEL T CO2 per 21.3 mmbtu, | COAL T CO2 per 21.3 mmbtu, | ETHANOL T CO2 per 21.3 mmbtu, | METHANOL | DME T CO2 per 21.3 |
| power plants | 2.818+00 | 12,608,974 | mmbtu,only production, no CCS | mmbtu,only production, CO2 harvest | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | NOT COUNTING UFECYCLE | mmbtu, NOT COUNTING LIFECYCLE | mmbtu, NOT COUNTING LIFECYCLE |
| # of 10 MW plants that can be run for 1 year, 45% | 3.218-05 | 143.9 | 1.93 | 0.68 | 1.23 | 1.65 | 1.48 | 1.68 | 2.42 | 0.33 | 1.80 | 1.80 |
| Equivalent # of 6 mtpa LNG train (BTU basis) | 6.87E-08 | 0.31 | | | | CASE | NOTES | | | | | |
| Tonnes LNG equivalent | 0.41 | 1,839,744 | Displacing 20% | i via blending (or p | oure ammonia) po | tentially saves a g | reat deal of mone | Υ. | | | | |
| Matrix Tanan | 1.04 | 4,666,667 | \$500/tonne ar | nmonia 20% chear | per than \$4/gal di | esel | | | | | | |
| Metric Tonnes coal equiv | | .,, | This could also | substantially assis | st on emissions (N | Ox. HC. PM). Pure | ammonia elimina | ates these emissio | ns (with, at worst | simple SCR) | | |
| Tonnes oil equivalent (TOE) | 0.500 | 2,243,590 | Ammonia blen | ds dilutes emission | ns and, likely, subs | tantially reduces I | HC/PM with optim | nization of engine | s (requires some r | esearch). | | |
| Tonnes resid equiv | 0.530 | 2,378,205 | Much simpler | to implement than | n LNG rail (distribu | ition, handling, fle | xibility for operat | ions/arbitrage, fu | el sourcing). For e | xample, | | |
| Gal LPG equiv | 234 | 1,050,000,000 | diesel/LNG ble | nding is not practi | cal. Fuel switchin | g on the same loc | omotive not pract | tical. | | | | |
| Gal Gasoline equiv | 172 | 771,794,872 | | | | | | | | | | |
| Gal Diesel equiv | 156 | 700,000,000 | | | | | | | | | 1 | |
| Price NH3 | | | | | | | | | | | | |
| | 0000 | | | | | | | | | | | |
| Total NH3 cost \$ | | 2,243,589,744 | | | | | | | | | | |
| Fuel cost for power, \$/kwh from NH3 | \$ 0.179 | | | | | | | | | | | |
| Price NATURAL GAS | \$10.00 | | | | | | | | | | | |
| Total Natural Gas cost \$ | | \$ 955,769,231 | | | | | | | | | | |
| Fuel cost for power for power, \$/kwh from gas | \$ 0.076 | | | | | | | | | | | |
| power, S/kwh from gas Price GASOLINE | | | | | | | | | | | | |
| | 54.00 | | | | | | | | | | | |
| Total Gasoline cost \$ | | \$ 3,087,179,487 | | | | | | | | | | |
| Fuel cost for power, \$/kwh from gasoline | \$ 0.313 | | | | | | | | | | | |
| Price LPG | \$4.00 | | | | | | | | | | | |
| Total LPG cost \$ | | \$ 4,200,000,000 | | | | | | | | | | |
| Fuel cost for power, | \$ 0.334 | | | | | | | | | | | |
| \$/kwh from LPG | - | | | | | | | | | | | |
| Price DIESEL | \$4.00 | | | | | | | | | | | |
| Total Diesel cost \$ | | \$ 2,800,000,000 | | | | | | | | | | |
| Fuel cost for power, S/kwh from diesel | \$ 0.284 | | | | | | | | | | | |
| Price COAL | \$100 | | | | | | | | | | | |
| Total Coal cost \$ | | \$ 466,666,667 | | | | | | | | | | |
| Fuel cost for power. | \$ 0.047 | | | | | | | | | | | |
| S/kwh from coal | | | | | | | | | | | | |
| | \$4.00 | | | | | | | | | | | |
| Price ETHANOL | _ | | | | | | | | | | | |
| Price ETHANOL Total Ethanol cost \$ | | \$ 4,541,025,641 | | | | | | | | | | |
| | \$ 0.361 | \$ 4,541,025,641 | | | | | | | | | | |

Railroad (displace diesel)

Diesel fuel is the major operating expense of long haul rail and is being challenged by increasingly stringent environmental regulations.

Displacing 20% via blending (or pure ammonia) requires about 4.5 MM TPA NH3 and potentially saves a great deal of money. \$500/tonne ammonia 20% cheaper than \$4/gal diesel

This could also substantially assist on emissions (NOx, HC, PM). Pure ammonia eliminates these emissions (with, at worst, simple SCR). Ammonia blends dilutes emissions and, likely,substantially reduces HC/PM with optimization of engines (requires some research).

Much simpler to implement than LNG rail (distribution, handling, flexibility for operations/arbitrage, fuel sourcing). For example, diesel/LNG blending is not practical. Fuel switching on the same locomotive not practical.



Global Markets - Overview

- Alaska (displace diesel across the state, supply Anchorage, alternate export market for Alaska gas)
- Hawaii (displace diesel, resid and gasoline across the islands)
- Northeast/MidAtlantic (energy security, grid stability, displace fuel oil)
- Midwest (energy security, grid stability, displace fuel oil/LPG)
- Caribbean (displace diesel, resid and gasoline across the islands)
- Japan (alternative to expensive LNG and coal, replacing nuclear)
- Indonesia (displace diesel, resid and gasoline across the islands)
- China (clean cities, rural access, much easier than gas)
- Europe (energy security, CHP, DG, fertilizer/fuel)
- Africa, South America (ammonia diesel gen, clean cities, rural access)



| | | RHOOD ENE | RGY STATIO | ON (LIKE A G | GAS STATIO | | | | ar Of Amm | onia | - | | | |
|--|-------------------|----------------------------------|---------------------------------------|---|--|---|--|---|---|--|--|--|--|--|
| USER INPUTS | ALL VALUES | ALL VALUES | | AMMONIA | NATURAL GAS | COST, TI | HERMO AND CO2 | DIESEL | COAL | ETHANOL | METHANOL | DME | | |
| CELLS | EQUIV 1 MT NH3 | CORRESPOND TO CASE PARAMETERS | | | | | | | | | INPUT Price of | | | |
| REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4 | 1.00 | 4,060 | | INPUT Price of NH3 delivered to site, \$ per tonne | INPUT Price of gas delivered to site, \$ / mmbtu | INPUT Price of gasoline delivered to site, \$ / gal | INPUT Price of LPG delivered to site, \$ / gal | INPUT Price of diesel delivered to site, \$ / gal | INPUT Price of coal delivered to site, \$ / tonne | INPUT Price of ethanol delivered to site, \$ / gal | methanol delivered to site, \$ / tonne | INPUT Price of DME delivered to site, \$ / tonne | | |
| OPTIONAL USER- OLFINED VARIABLE ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NHS GASS) IN CS. ITERATE DA TO ACHEVE DESIRED QUANTITY IN DS | | 0.00 | | \$350 | \$15.00 | \$3.00 | \$2.00 | \$3.80 | \$50 | \$3.00 | \$200 | \$290 | | |
| MMBTU (or 1000 CF gas equiv) contained in NH3 | 21.32 | 86,558 | | | MMBTU gas for 21.3 MMBTU | Gal gasoline for 21.3 MMBTU | Gal LPG for 21.3 MMBTU | Gal diesel for 21.3 MMBTU | Tonnes coal for 21.3 MMBTU | Gal ethanol for 21.3 MMBTU | Tonnes methanol for 21.3 MMBTU | Tonnes DME for 21.3 MMBTU | | |
| MMBTU gas required for NH3 | 32.0 | 129,930 | | 14 | 21.1 | 172 | 234 | 156 | υ | 25 | 0.982 | 0.71 | | |
| TCF natural gas required for NH3 | 2.946-08 | 0.000 | | NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario | Gas Fuel Cost (for 21.3 mmbtu) - This Scenario | Gasoline Fuel Cost (for 21.3 mmbtu) - This | LPG Fuel Cost (for 21.3 mmbtu) - This Scenario | Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario | Coal Fuel Cost (for 21.3 mmbtu) - This Scenario | Ethanol Fuel Cost (for 21.3 mmbtu) - This | Methanol Fuel Cost (for 21.3 mmbtu) - | OME Fuel Cost (for 21.3 mmbtu) - This | | |
| Tonnes water produced from NH3 | 1.588+00 | 6,415 | | melbuj - Thi Scenario | | | | | | | | | | |
| # Global ammonia | 6.672-09 | 0.000 | | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 35% efficiency (coal like) | kwh from 21.3 mmbtu at 35% efficiency (coal like) | 45% efficiency (gas/nh3 | kwh from 21.3 mmbtu at 45% | kwh from 21.3 mmbtu at 45% | | |
| If of World Scale NH3 | 1.258-06 | 0.01 | | 184 <u>0)</u> 2800 | 18ke) 2800 | 2200 | 18ke) 2800 | 2200 | 220 | like) 280 | efficiency (gas/nh3 | efficiency (gas/nh3 2800 | | |
| Number of 60,000 cbm | 2.448-05 | 0 | | Fuel cost for power, S/kwh from NH3 | Fuel cost for power for power, S/kwh from gas | Fuel cost for power, S/kwh from gasoline | Fuel cost for power, \$/kwh from LPG | Fuel cost for power, S/kwh from diesel | Fuel cost for power, S/kwh from coal | Fuel cost for power, S/kwh from coal | Fuel cost for power, S/kwh from | Fuel cest for power, S/kwh from DME | | |
| Number of 80 tonne | 0.0125 | 51 | | 5/xwh from Nin3 | power, 5/kwn trom gas | \$0.235 | \$0.167 | \$0.269 | Syntech from coal | 50.271 | methanol \$0.070 | S0.074 | | |
| railcar deliveries | 1.005.06 | 0.0 | AMMONIA, NO | AMMONIA w/ | NATURAL GAS | GASOLINE | LPG | DIESEL | COAL | ETHANOL | METHANOL | DME | | |
| pipeline MWh from 45% efficient | 2.815+00 | 11,410 | CCS T CO2 per 21.3 | HARVEST T CO2 per 21.3 | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 mmbtu, | T CO2 per 21.3 | T CO2 per 21.3 | | |
| power plants | 3.218-05 | 11,410 | production, no CCS | CO2 harvest | LIFECYCLE | UFECYCLE | LIFECYCLE | LIFECYCLE | UNICYCLE | | COUNTING LIFECYCLE | COUNTING LIFECYCLE | | |
| can be run for 1 year, 45% | | | 1.93 | 0.68 | 1.23 | | | 1.68 | 2.43 | 0.33 | 1.80 | 1.80 | | |
| Equivalent # of 6 mtpa LNG train (BTU basis) | 6.875-08 | 0.00 | Local Energy St | ation Dispensing | 1 75 Mm Gale Pa | r Year Of Ammoni | NOTES | | | | | | | |
| Tonnes LNG equivalent | 0.41 | 1,665 | 2.53 | | | ispense 1.5 MM ga | | arader of aaroling | diaral in a year | This case | | | | |
| Metric Tonnes coal equiv | 1.04 | 4,223 | examines a 'nei | ighborhood' amm | onia energy statio | on of approximate rban environment | ly the same scale | that could provide | e power and heat | to the | | | | |
| Tonnes oil equivalent (TOE) | 0.500 | 2,030 | ammonia. The | prototype for thi | s is the MHI Mega | Ninja gas-driven g | enset (delivered o | on 40' trailer, 1.5 M | WW generator op | erating at 42.5% | | | | |
| Tonnes resid equiv | 0.530 | 2,152 | efficiency, desig adsorptive air c | gned for combine conditioning.) | d heat/power tak | ing efficiency up to | o 75% for medium | pressure steam/ | space and water h | neating and | | | | |
| Gal LPG equiv | 234 | 950,116 | | | | less than a gasoli | | | | | | | | |
| Gal Gasoline equiv | 172 | 698,376 | instead of retail and fuel deliver | l interface with h ry logistics would | undreds of transa be similar. | ctions to untrained | d public per day). | But tank volume, | general regulator | ry requirements | | | | |
| Gal Ethanol equiv | 253 | 1,027,262 | The average we | eekly volume wou | ld be about 35,00 | 0 gallons. We can | 'design' for 40,00 | 00 gal/week peak | usage. A typical t | ank size for | | | | |
| Gal Ethanol equiv | 253 | 1,027,262 | The average we | ekly volume wou | ld be about 35,00 | 0 gallons. We can | 'design' for 40,00 | 00 gal/week peak | usage. A typical t | ank size for | | | | |
| Price NH3 | \$350 | | ammonia distri temp/pressure | butors is 30,000 g maintenance), w | allons. So, with o could operate w | ine 30,000 gal tank with three a week d | (installed underg leliveries from 11, | ground for safety, 500 gal tank truck | security and ease | of | | | | |
| Total NH3 cost \$ | | 1,421,114 | I'm sure the log | istics can/will be | optimized beyond | i that, but this will | do for illustration | n. | | | | | | |
| Fuel cost for power, | \$ 0.125 | | Very rough pro Roughly \$1.5-\$ | | be about \$1.2 MM | A for ammonia M | egaNinja, \$0.1 MI | M for undergroun | d tank, connectio | ons and land. | | | | |
| Price NATURAL GAS | \$15.00 | | With these deli | very assumptions | (1.75 MM gal am | monia/year), a 1.5 | MW Meganinia | can be supplied 85 | 5% of the time (.1 | 3/.15). The unit | | | | |
| Total Natural Gas cost \$ | | \$ 1,297,274 | would be availa model this as | ble 100% of the t | ime (minus maint | enance) and could | be run at the cos | t of more frequer | nt ammonia delive | ries. We can | | | | |
| Fuel cost for power for power, S/kwh from gas | 5 0.114 | | | is integrated into | the local electric | al grid, sells exces | nower into the g | rid and buys now | er from the grid w | then nower is | | | | |
| power, S/kwh from gas | \$3.00 | | offered at below | w cost/value of lo | cal power and he | at supply. For example at power demain | mple, buying low | cost base load pov | | | | | | |
| Total Gasoline cost \$ | | \$ 2,095,128 | M | 10. 16 5 | 6 | for 7450 hrs for 1 | | | of CHP heat (cr.)- | lated as 209. of | | | | |
| Fuel cost for power, | | 2,095,128 | | | | e will assume con: | | | | | | | | |
| S/kwh from gasoline | \$ 0.235 | | | | | | | | | | | | | |
| Price LPG | \$2.00 | | | 1.75 mm tonnes | | | | | | | | | | |
| Total LPG cost \$ | | \$ 1,900,232 | residential cust | omers (especially | conservative in th | environments, the he winter). Sales (| or avoided costs o | of gas/power purc | hases) of the pow | | | | | |
| Fuel cost for power, S/kwh from LPG | \$ 0.167 | | | | | .57 MM for powe | | | | | | | | |
| Price DIESEL | \$3.80 | | year that kwh a | re valued at high | er than \$0.11 per | even rejecting all t kwh, the generato | r can be operated | for additional pr | ofit. For example | in New | | | | |
| Total Diesel cost \$ | | \$ 2,406,961 | England/Middle | e Atlantic region, | retail electricity p | rices are uniformly at a margin of \$0.1 | above \$0.16 per | kwh. So, if we ar | e running a 1500 | kw unit for 15% | | | | |
| Fuel cost for power, S/kwh from diesel | \$ 0.269 | | | | | iness blind (i.e, sel | | | | power sales | | | | |
| Price COAL | 550 | | loosely) Fuel cost at \$30 | | | | | | | | | | | |
| Total Coal cost \$ | | \$ 211,137 | Revenues from | 85% base operat | ions (contracted a | t conservative pri- | | | | | | | | |
| Fuel cost for power, S/kwh from coal | \$ 0.024 | | | gin of \$680,000 to | | | + - > 0,000 | | | | | | | |
| Price ETHANOL | \$3.00 | | Upside potentia | al on these reven | Jes. | | | | | | | | | |
| Total Ethanol cost \$ | | \$ 3,081,787 | | Capacity payments from PJM RPM (market to pay for guaranteed capacity in PJM grid). In New York, this is about \$200 per MW (paid whether the unit is running or not). This is \$73,000 per year. | | | | | | | | | | |
| Fuel cost for power, | \$ 0.271 | | | | | | | - Balland | | | | | | |
| S/kwh from ethanol MegaTonnes CO2 saved with NH3 with harvest vs | 5.508-07 | 0 | | | | n the grid (this pov ent, price spikes fi | | | provided power (| no rísk from gas | | | | |
| GAS | | 0 | | | | | | | | | I | | | |

Local Energy Station Dispensing 1.75 Mm Gals Per Year Of Ammonia

A typical high volume gasoline station can easily dispense 1.5 MM gallons of multiple grades of gasoline/diesel in a year. This case examines a 'neighborhood' ammonia energy station of approximately the same scale that could provide power and heat to the neighborhood (or condo or office building) in an urban environment. This station would house a diesel genset/CHP unit running on ammonia. The prototype for this is the MHI MegaNinja gas-driven genset (delivered on 40' trailer, 1.5 MW generator operating at 42.5% efficiency, designed for combined heat/power taking efficiency up to 75% for medium pressure steam/space and water heating and adsorptive air conditioning.)

The general complexity of these stations would be less than a gasoline station (single grade, dispensed almost entirely to the generators instead of retail interface with hundreds of transactions to untrained public per day). But tank volume, general regulatory requirements and fuel delivery logistics would be similar.

The average weekly volume would be about 35,000 gallons. We can 'design' for 40,000 gal/week peak usage. A typical tank size for ammonia distributors is 30,000 gallons. So, with one 30,000 gal tank (installed underground for safety, security and ease of temp/pressure maintenance), we could operate with three a week deliveries from 11,500 gal tank trucks (typical size ammonia trucks). I'm sure the logistics can/will be optimized beyond that, but this will do for illustration.



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- Very rough project costs would be about \$1.2 MM for ammonia MegaNinja, \$0.1 MM for underground tank, connections and land. Roughly \$1.5-\$2 MM.
- With these delivery assumptions (1.75 MM gal ammonia/year), a 1.5 MW Meganinja can be supplied 85% of the time (.13/.15). The unit would be available 100% of the time (minus maintenance) and could be run at the cost of more frequent ammonia deliveries. We can model this as
- A CHP unit that is integrated into the local electrical grid, sells excess power into the grid and buys power from the grid when power is offered at below cost/value of local power and heat supply. For example, buying low cost base load power at night from utility based on TOD pricing and operating during the day to ease peak power demand on the utility's peakers)
- Runs 85% of the time routinely (providing 1.5 MW for 7450 hrs for 11,200,000 kwh and 26,000 mmbtu of CHP heat (calculated as 30% of the mmbtu's in the 1.75 mm gal of ammonia)). We will assume conservatively that 15,000 mmbtu of that heat would be effectively used or sold.
- At \$300/tonne, 1.75 mm tonnes of ammonia costs \$1.2 MM
- If we assume New England/Middle Atlantic urban environments, then \$0.14 per kwh and \$14 per MMBTU are conservative prices for residential customers (especially conservative in the winter). Sales (or avoided costs of gas/power purchases) of the power and CHP heat from 85% operation at these prices would yield \$1.57 MM for power and \$0.21 MM for heat for a total of \$1.78 MM.
- At \$300/tonne ammonia, the fuel cost for power (even rejecting all the CHP heat) is \$0.107 per kwh. So, for the additional 15% of the year that kwh are valued at higher than \$0.11 per kwh, the generator can be operated for additional profit. For example, in New England/Middle Atlantic region, retail electricity prices are uniformly above \$0.16 per kwh. So, if we are running a 1500 kw unit for 15% of a year (1300 hrs), we are selling 2,000,000 kwh at a margin of \$0.05 (bringing in \$100,000 extra revenue).
- Overview on very rough numbers running the business blind (i.e, selling at average prices, managing CHP heat and extra power sales loosely)
- Fuel cost at \$300/tonne \$1,200,000
- Revenues from 85% base operations (contracted at conservative prices) \$1,780,000
- Opportunistic sales of power for other 15% of generating capacity \$100,000
- Operating margin of \$680,000 to cover capex/opex/profit.



- Upside potential on these revenues.
- Capacity payments from PJM RPM (market to pay for guaranteed capacity in PJM grid). In New York, this is about \$200 per MW (paid whether the unit is running or not). This is \$73,000 per year.
- Potential payments from reliability premiums from the grid (this power is much more reliable than grid provided power (no risk from gas deliverability, downed power lines, frozen equipment, price spikes from hot summer afternoons, etc).
- Well positioned availability of reliable power can be very valuable during high stress in the grid (prices have spiked above \$1000/MWh and \$100 per mmbtu on several occasions over the last few years). This value can be captured via market/auction transactions on advanced grid markets like RPM or through opportunistic transactions in real time.
- Upside revenue potential for similar projects in other regions of the world. Examples:
- Island economies that must generate their power from fuel oil (Hawaii, Caribbean, Indonesia). Fuel oil is \$30-\$40 per mmbtu. It is dirty and must be located away from populations (and especially resorts). That also makes it very difficult to capture and utilize the 1/3 of the btu's from CHP that clean ammonia engines can provide. These units can provide clean power at less than half the cost and, on top of that, very efficient heat and air conditioning (absorptive chilling).
- Medium scale distribution/retail (frozen/refrigerated foods), light industry and agriculture utilizing refrigeration, medium pressure steam or drying (e.g., crops) that place high value on the associated heat)
- Regions that place high value on pure water (exhaust from ammonia MegaNinja is water and nitrogen. Pure water can be captured at the cost of condensing the water.) Combustion of 1.75 MM gallons of ammonia generates about 1.7 MM gallons of water.
- They will be very attractive to sites willing and able to pay large premiums for locally controlled, uninterruptible power (financial/business centers, server farms, hospitals.
- military/government installations, large research facilities/research universities)
- Regions that are imposing a cost on CO2 emissions (e.g., California) can reduce or eliminate those costs.



- This is potentially a very positive development for utilities, local/regional government (e.g., PJM and RPM) for:
- Predictable standby reserve available on 5 minute call-up (with right incentives and minimally sophisticated 'smart grid' controls) (much cheaper and much more flexible than spinning reserve CCGT that is only used as gas prices are rising above \$40/mmbtu)
- Distributed and potentially very substantial regional fuel reserve for mid-winter, late summer, regional security (much cheaper (pseudo-'free') than natural gas storage and much more flexible)
- This is potentially a very positive development for property managers and energy customers
- More predictable/controllable pricing through contract and/or arbitrage at regional or urban level with ammonia producers/gas monetizers. And significantly lower than market prices over the last five years.
- Lots of headroom for optimization for profits. Project design for medium pressure steam, space heating, hot water heating, drying operations (e.g., crops), heat driven chillers (air conditioning, refrigeration for food distribution and retailing)
- This is potentially a very positive development for urban governments
- Distributed, secure energy storage for reliable power within the city
- Very clean power generation (zero carbon as well as zero traditional pollutants)
- Initial infrastructure for ammonia fuel for buses, delivery trucks, taxis, govt vehicles etc for superclean transport in cities (much cheaper than CNG or electric, much, much cheaper than hydrogen)



How Does This All Get Started?

- Market demonstration at 1-10 MW scale (diesel gen, refit, new optimized, blends)
- Tech/market demo at 25-50 MW scale (repowering coal/fuel oil boilers)
- Engage ammonia producers/investors
 - New build guaranteed offtake (some fraction of production)
 - Eventually, utility plants with guaranteed returns for fuel take or pay (with perhaps shared profits for joint sales into market after satisfaction of energy market contractual requirements)
 - Market, regulatory, technology demo support from self selected producers
 - Plant technology/engineering firms (KBR, Uhde, MHI, etc) that will benefit from increased building
- Low cost, high CO2 value areas for low carbon, low cost fuels
- Accelerate demo/commercialization of power to NH3 technologies
 - Compile list of potentially interested investors, green funding, etc for incipient technologies for investments in the range of \$5-\$20 MM for FEED, critical demoes or initial deployment in regions for low cost "stranded" power (i.e., Canada, Iceland)
 - Competition for proposals for ammonia from power, perhaps with funding from such entities (NH3Fual Association as clearinghouse??)
- Future Search with engaged stakeholders sponsored by CATF

