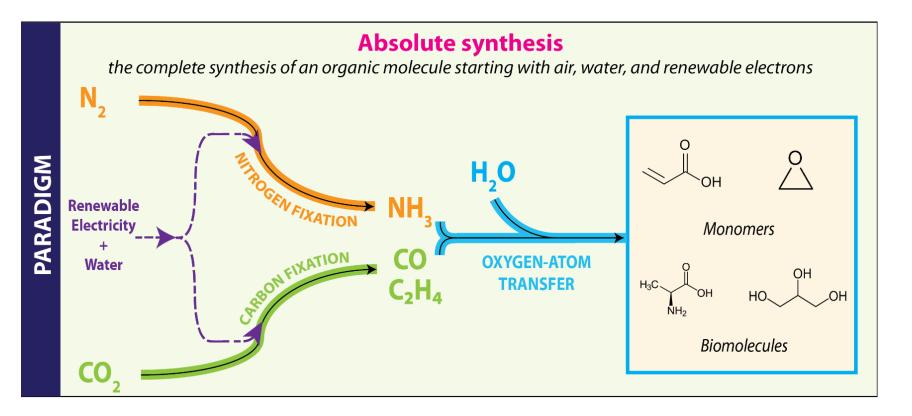
Electrification of Ammonia Synthesis

Prof. Karthish Manthiram

Department of Chemical Engineering Massachusetts Institute of Technology

> Email: karthish@mit.edu Website: manthiramlab.com

Manthiram Lab: Electrifying and decarbonizing chemical transformations



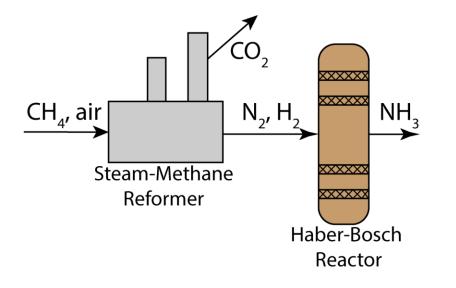
Air, water, and renewable electrons are distributed, sustainable resources

Electrical potential enables mild conditions of operation, replacing temperature and pressure

Our lab has developed new catalysts and integrated processes for electrically-driven ammonia synthesis, carbon dioxide fixation, and plastic production

Ammonia production is trending towards electrochemistry

Traditional Haber-Bosch



Replacing pressure with voltage 1/2 N₂ + 3/2 H₂ \rightarrow NH₃



Schiffer

Conversion Thermochemical **Electrochemical** At ambient pressure (1 atm): Х Х 400 0.4 X > 99% •+• 350 0.35 Voltage also 0.8 0.8 improves kinetics, 300 0.3 so can operate at Lressure (atm) 250 200 150 lower X <20% $\sum^{0.25}$ 0.6 0.6 temperature 0.2 Voltage (Higher pressures to 0.4 0.4 achieve reasonable Apply 100 conversions 0.1 voltage to 0.2 0.2 increase 50 0.05 conversion 0 0 0 0 400 200 600 800 200 400 600 800 0 0 Temperature (°C) Temperature (°C) Higher temperatures to achieve

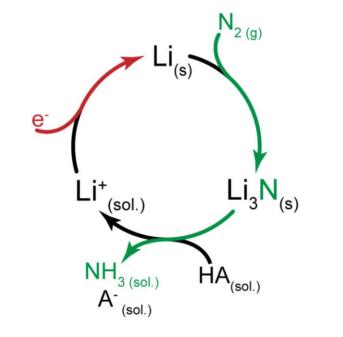
reasonable rates

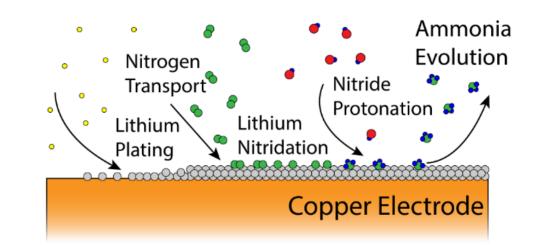
Z. J. Schiffer and K. Manthiram Joule 1 10-14 (2017).

Lithium mediated ammonia synthesis



Nikifar Lazouski



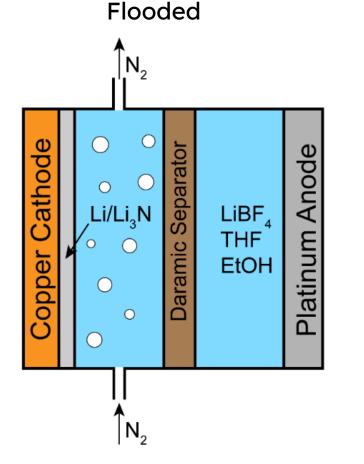


Cycle involving electrochemical and thermochemical steps

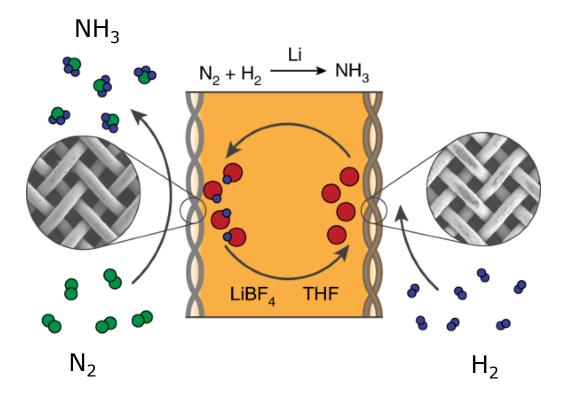
Reactions occur continuously at electrode surface

Fichter, P. G. F, Erlenmeyer, H. *Helv. Chim. Acta* (1930) Tsuneto, A. J. *Electroanal. Chem.* (1994) N. Lazouski, Z. J Schiffer, K. Williams, and K. Manthiram, *Joule* 3, 1127-1139 (2019).

Overcoming transport limitations and undesired overall reaction



Gas diffusion electrodes



Rates limited by transport, undesirable proton source, and low energy efficiency

Gas diffusion electrodes to enable $N_2 + 3H_2 \rightarrow 2NH_3$

Rates of ammonia synthesis above the flooded transport limit

NH₃ Faradaic efficiency (%)

50

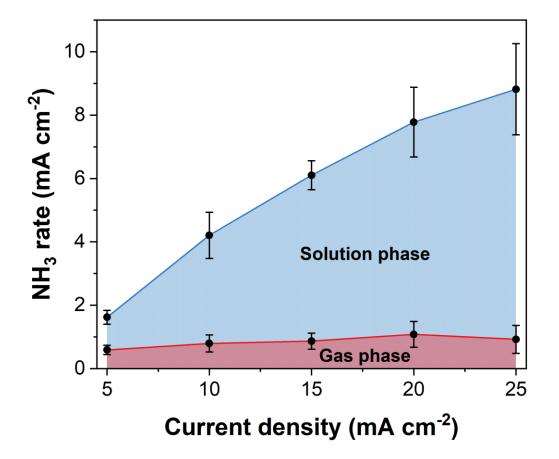
40

30

20

10

0.0



The rate of nitrogen reduction is increased significantly, with some produced ammonia found in the gas phase High FEs can be obtained at 15 mA cm⁻² at non-zero pressure gradients across the GDE

N₂ pressure gradient (kPa)

0.5

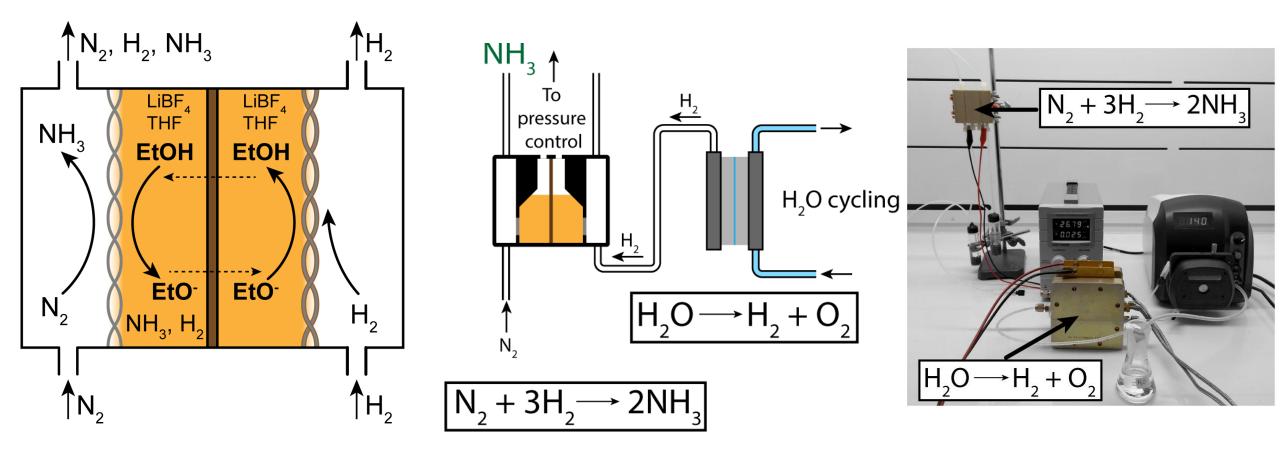
Solution phase

Gas phase

1.0

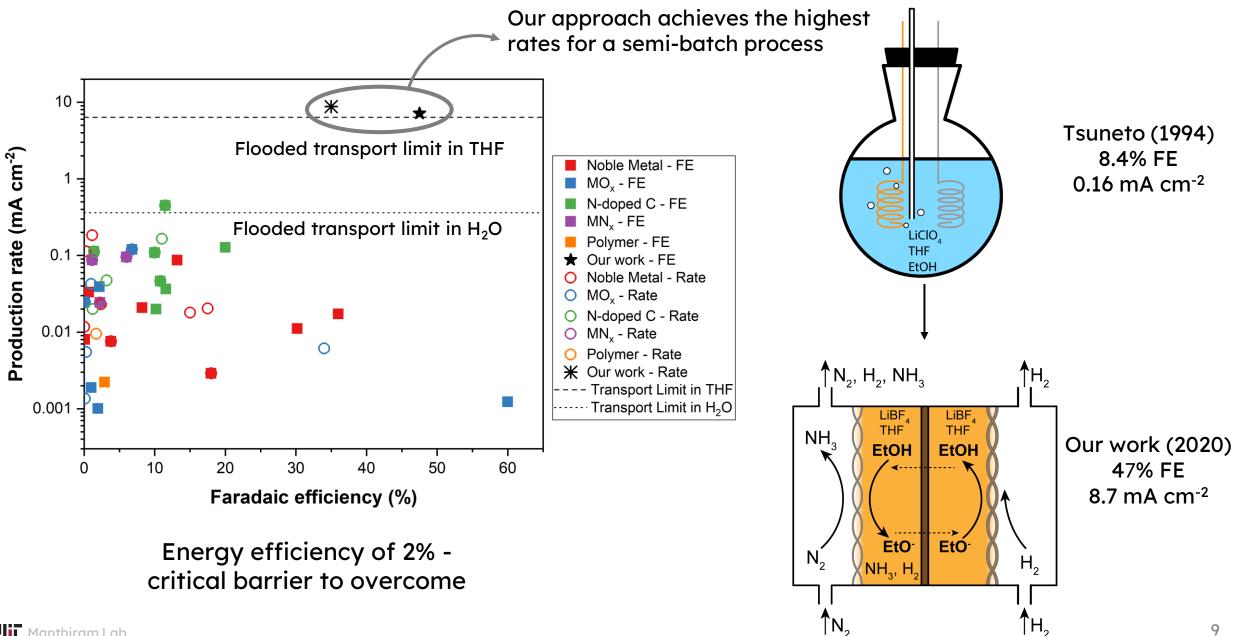
1.5

Coupling to water splitting



Hydrogen oxidation at the anode can replenish protons in the electrolyte Water splitting-derived hydrogen can be used at the anode to have overall ammonia production from N_2 and H_2O

Comparing our system to reported catalysts



Acknowledgements



Aditya

Limaye



Joy Zeng





Dengtao Yang



Zachary Schiffer





Kindle Williams

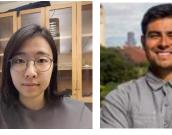




Nathan Corbin



Chung



Joseph Maalouf



Glen Junor





manthiramlab.com



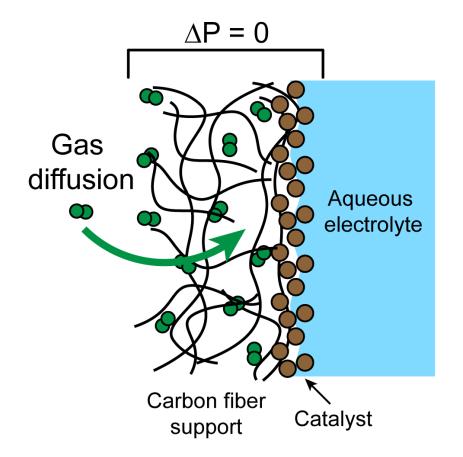
@ManthiramLab @KManthiram

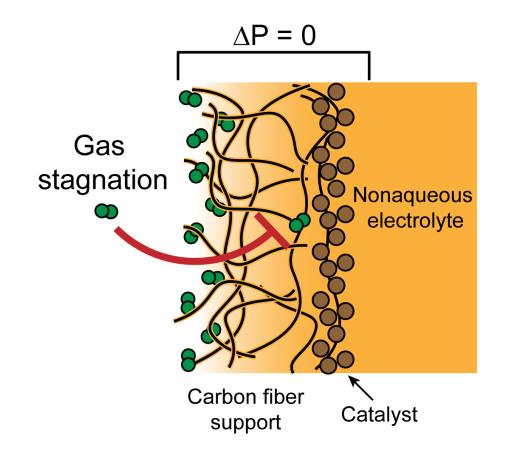


Kyoungsuk

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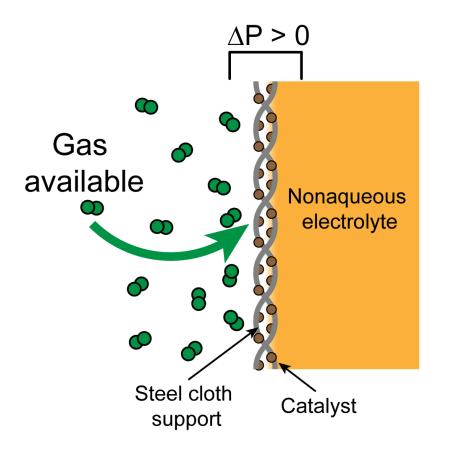
Conventional gas diffusion electrodes are not viable

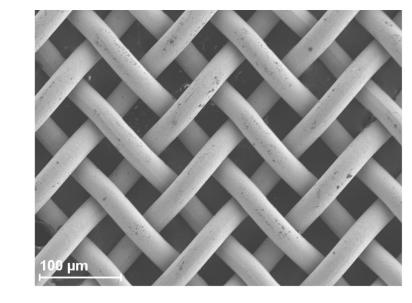




A stable gas-liquid interface, stabilized by hydrophobic interactions, can increase gas transfer rates Hydrophobic interactions are absent in nonaqueous electrolytes, leading to electrode flooding and loss of gas-liquid interface

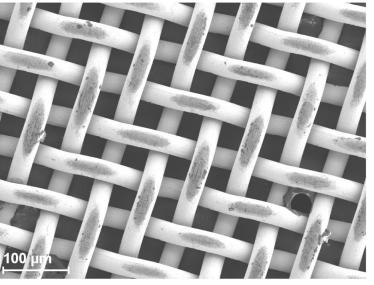
Using metallic meshes can overcome flooding





Stainless steel cloths can be used as GDEs directly for nitrogen reduction

Catalysts can be deposited for use in other chemistries



Gas-liquid interface at metallic mesh support allows for rapid transport; metal meshes don't pull in electrolyte by capillary action due to less favorable surface interactions

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